

CO2 Injection for Methane Production from Hydrate Reservoirs

by

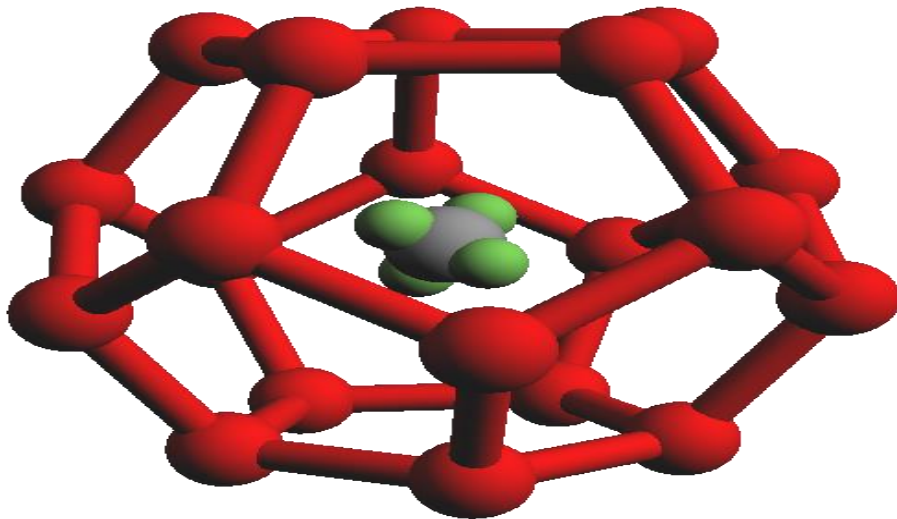
A. Graue, G. Ersland and S. Almenningen

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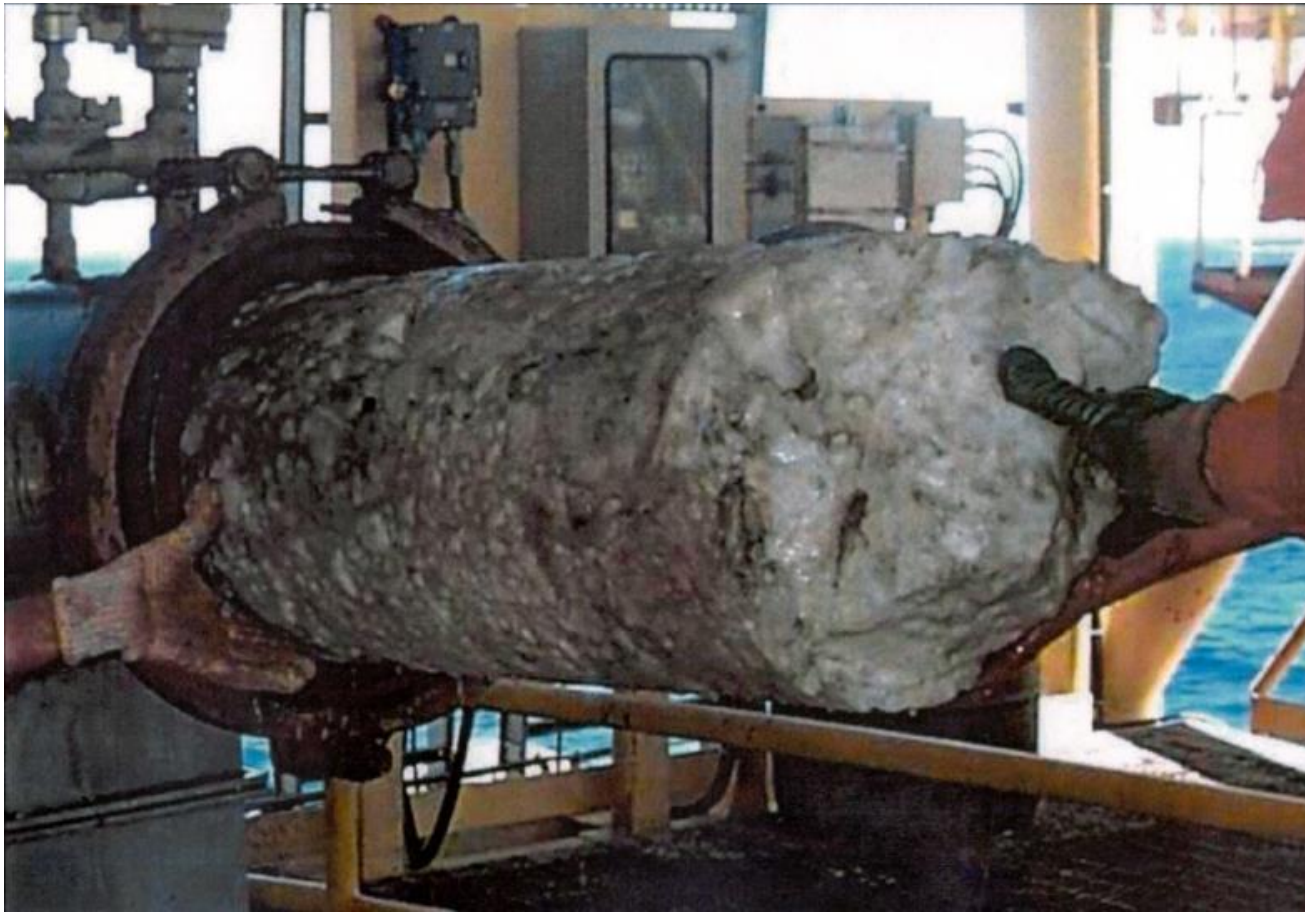
GAS HYDRATES

- Solid state of gas and water where the water molecules form a cavity that encapsulates the guest molecule.



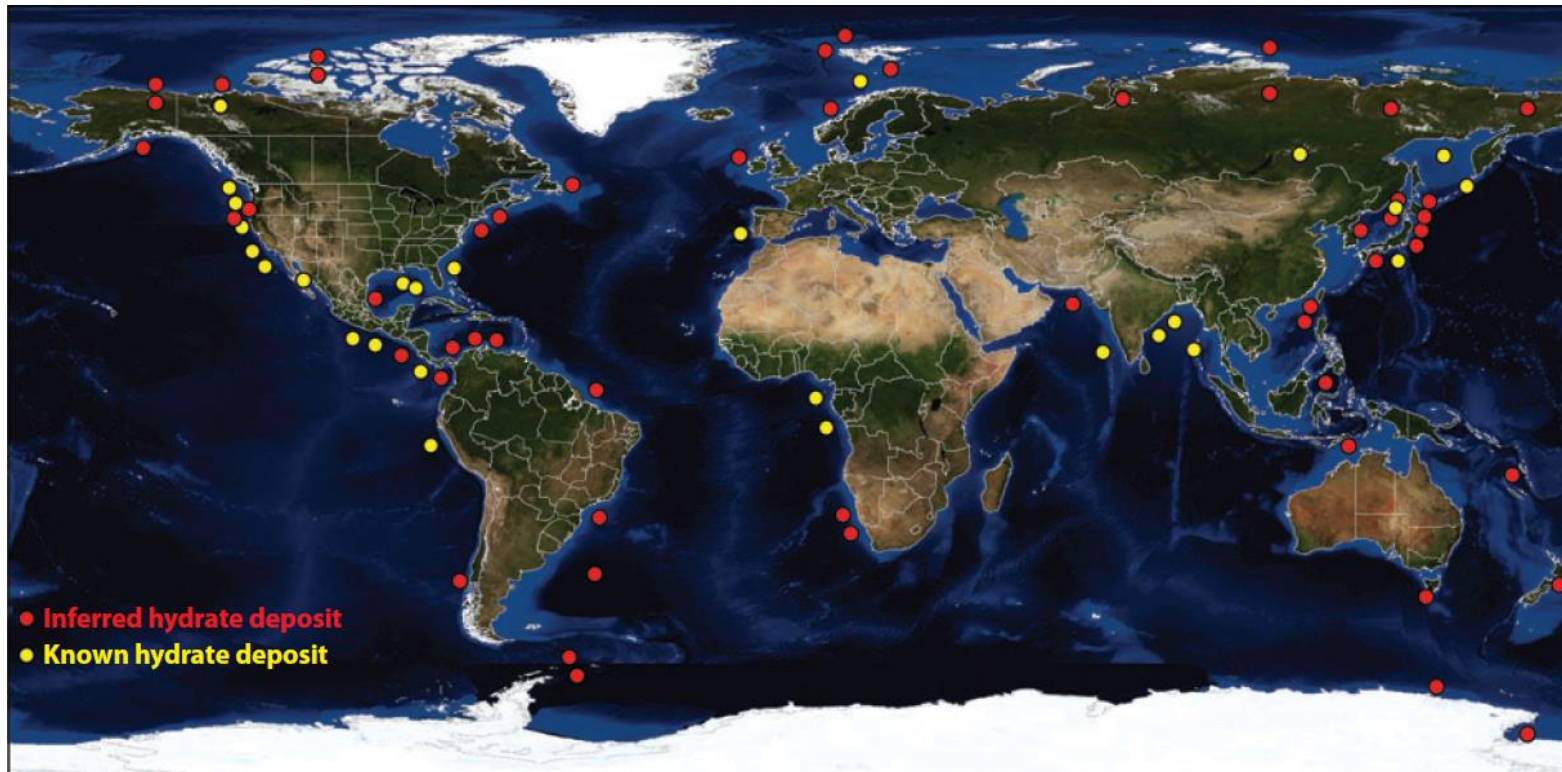
Why are hydrates of interest?

- Initial interest as a curiosity
- Plugging of production and transportation pipelines



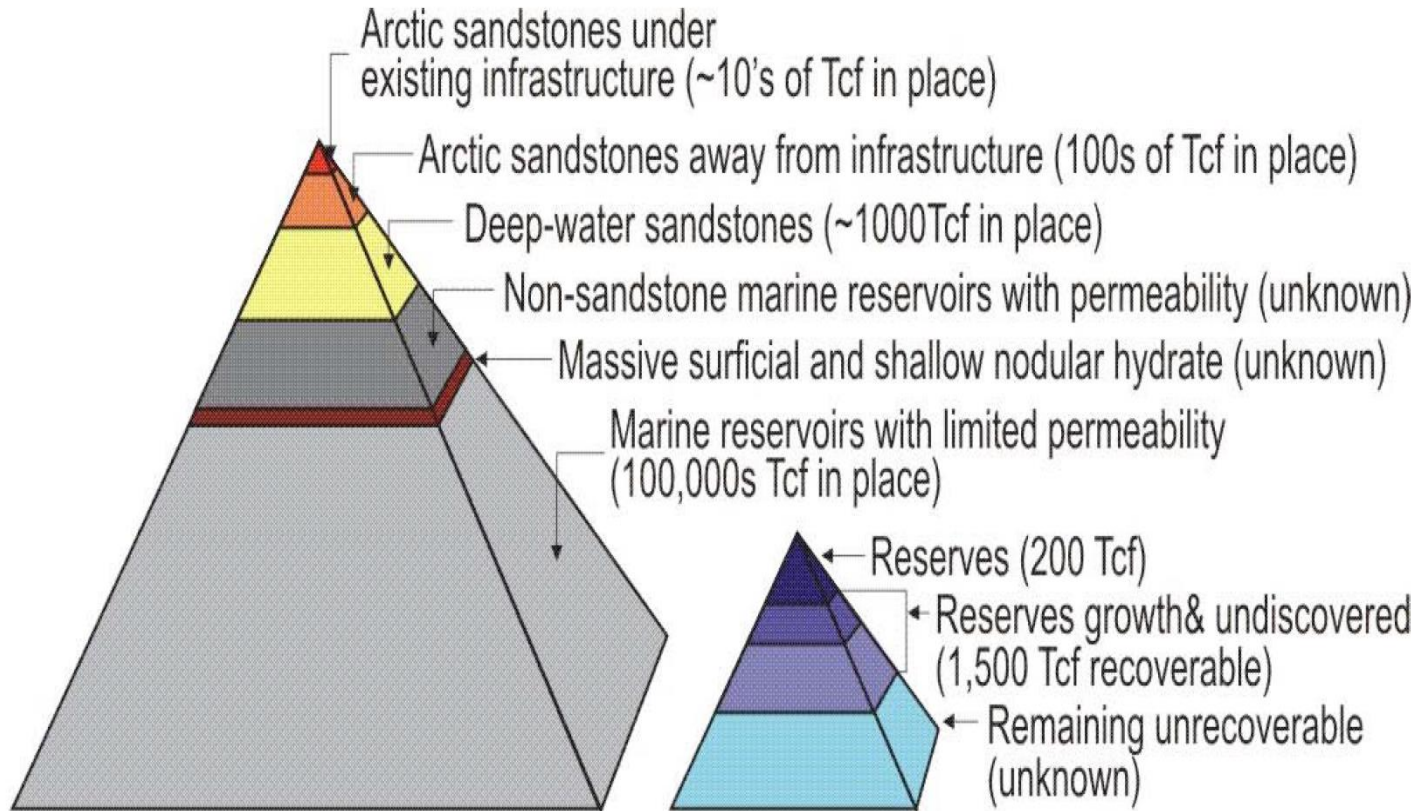
Renewed interest

- Significant amount of energy
 - Permafrost regions
 - Marine environments (high water column)



Hydrate as Energy Resource

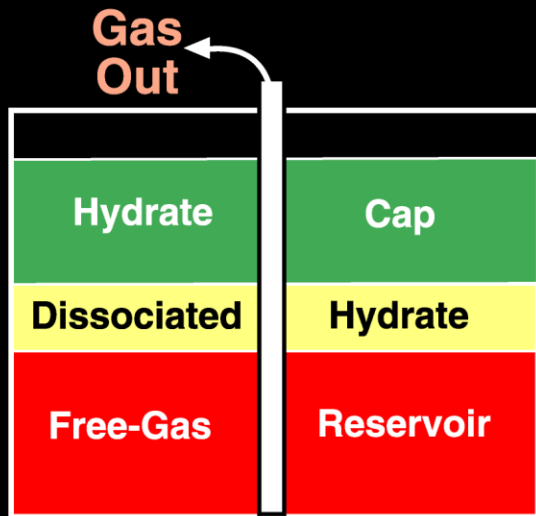
Ref.: Fire in the Ice, U.S. Department of Energy • Office of Fossil Energy • National Energy Technology Laboratory



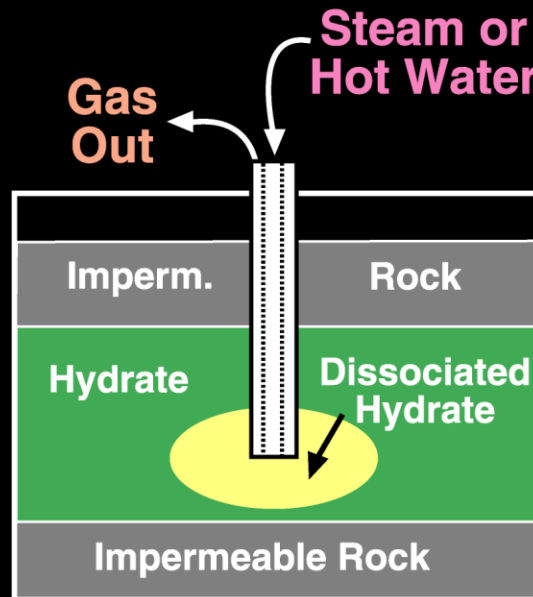
Gas Hydrates Resource Pyramid (left). To the right is an example gas resources pyramid for all non-gas-hydrate resources.

Gas Hydrate Production Methods

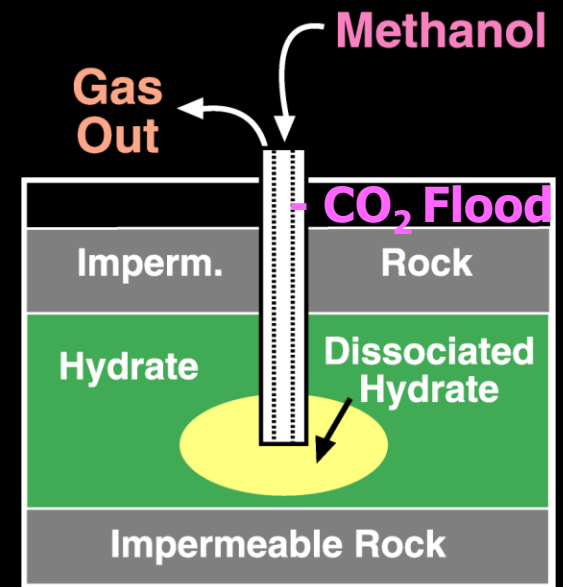
Depressurization



Thermal Injection



Inhibitor Injection



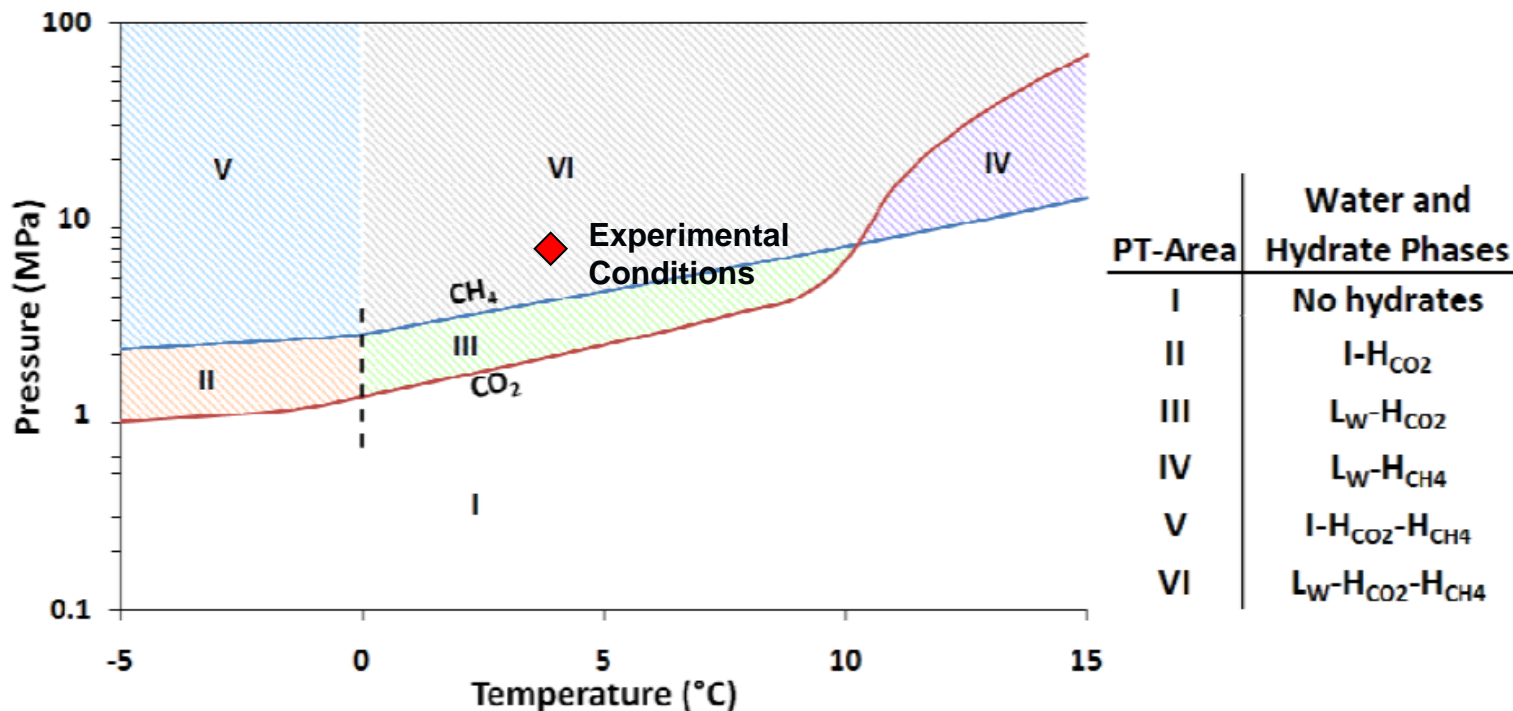
Modified from "GAS HYDRATES OF NORTHERN ALASKA", January 2005

Evaluation of Alaska North Slope Gas Hydrate Energy Resources: A Cooperative Energy Resource Assessment Project
US Bureau of Land Management, US Geological Survey, & State of Alaska Division of Geological and Geophysical Surveys

Bob Fisk, USBLM, Anchorage, Alaska, Tim Collett, USGS, Denver, Colorado & Jim Clough, DGGS, Fairbanks, Alaska

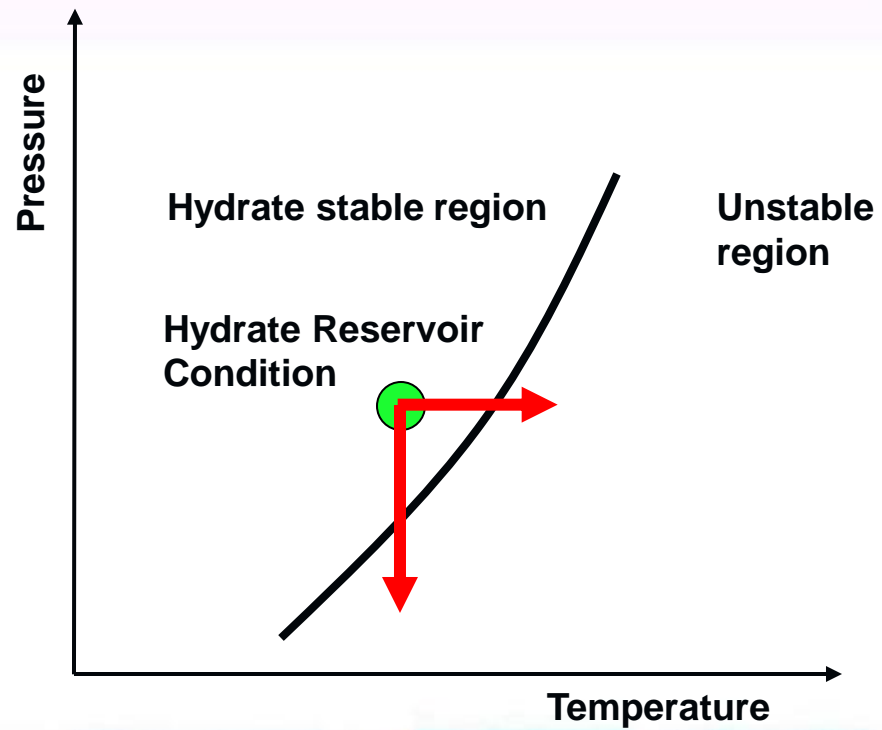
CH₄ PRODUCTION INDUCED BY CO₂ INJECTION

- Provides thermodynamically more stable gas hydrate than CH₄



GAS HYDRATE PRODUCTION METHODS

- Move the gas hydrate outside its stability region
 - Depressurization
 - Thermal stimulation
 - Hydrate inhibitors
- **CO₂ exchange**



CO₂ Exchange: Project Motivation

- **The amount of energy bound in hydrates may be more than twice the world's total energy resources in conventional hydrocarbon reservoirs; i.e. oil-, gas- and coal reserves**
- **Simultaneous CO₂ Sequestration**
- **Win-win situation for gas production**
- **Need no hydrate melting or heat stimulation**
- **Spontaneous process**
- **No associated water production**
- **Formation integrity**

**CO₂ storage in hydrates
with associated methane
gas production**

Challenge:

**Determine exchange mechanisms during potential
sequestration of CO₂ to produce methane from hydrates**



Three component Phase Field Theory

$$F = \int d\mathbf{r} \left\{ \frac{\varepsilon^2 T}{2} (\nabla \phi)^2 + \sum_{i,j=1}^3 \frac{\varepsilon_{i,j}^2 T}{4} (c_i \nabla c_j - c_j \nabla c_i)^2 + f_{bulk}(\phi, c_1, c_2, c_3, T) \right\}$$

$$f_{bulk} = wTg(\phi) + [1 - p(\phi)]f_S(c_1, c_2, c_3, T) + p(\phi)f_L(c_1, c_2, c_3, T)$$

$$\dot{\phi} = -M_\phi \frac{\delta F}{\delta \phi} + \zeta_\phi$$

$$\sum_{i=1}^3 c_i = 1$$

$$\dot{c}_i = \nabla M_{c_i}(c_1, c_2, c_3) \nabla \left(\frac{\delta F}{\delta c_i} - \zeta_i \right)$$

Parameters ε and w can be fixed from the interface thickness and interface free energy. ε_{ij} set equal to ε

CO₂ Storage in Hydrate Reservoirs with Associated Spontaneous Natural Gas Production

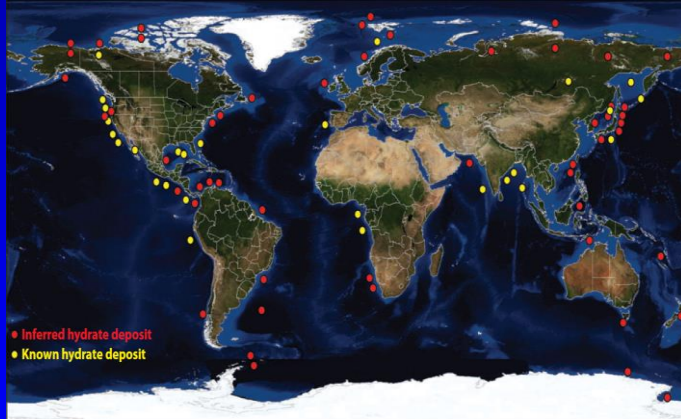
Arne Graue and Bjørn Kvamme, Dept. of Physics, University of Bergen, NORWAY
Funding: ConocoPhillips, Statoil and The Research Council of Norway



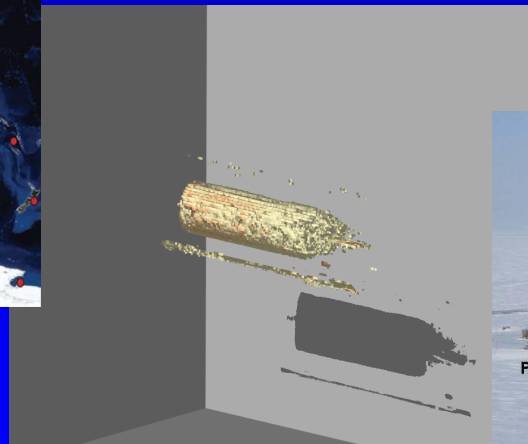
Objectives:

Experimentally and theoretically determine spontaneous methane production when hydrate is exposed to CO₂; with the purpose of CO₂ sequestration.

Methane hydrate reservoirs



In-Situ imaging (MRI) of hydrate formation



Methane production by CO₂ injection in field test in Alaska 2012



Summary of Field Test (Injection Test)

Schedule:

Apr. 2011: Drilling test well (Complete)
Nov. 2011: Finalizing parameters for the field test
Jan.-Apr. 2012: Field test

Location : Prudhoe Bay operating unit in Alaska, USA
Operator : ConocoPhillips Company (COP), through its wholly owned subsidiary, ConocoPhillips Alaska, Inc.
Investors : The United States Department of Energy (DOE)
JOGMEC; Japan Oil, Gas and Metals National Corp.

BEAUFORT SEA



Greater
Kuparuk
Area

Greater
Prudhoe Area

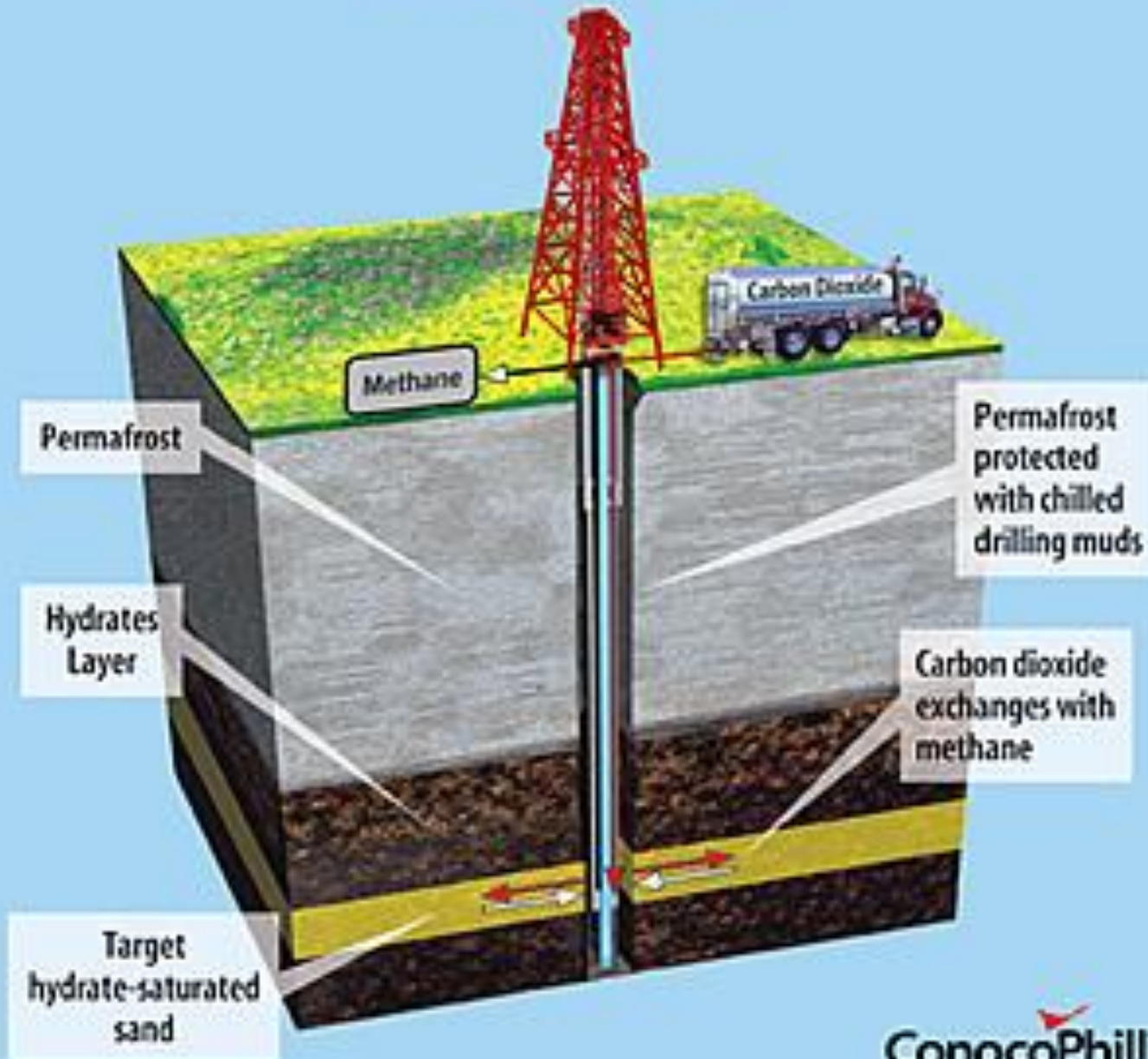
Trans-Alaska Pipeline

Potential Gas Hydrate Accumulations
Source: USGS



ConocoPhillips

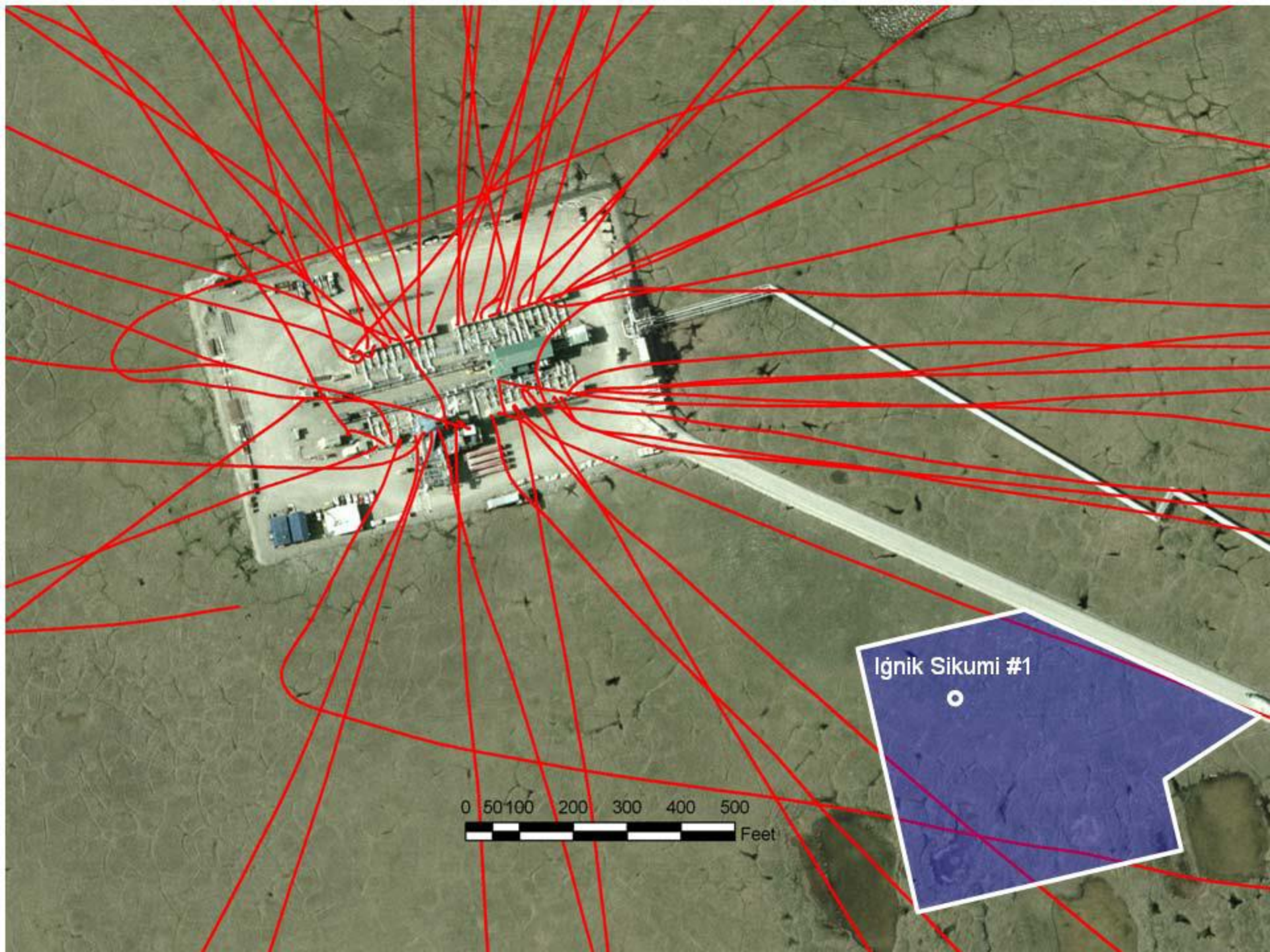
Methane Hydrates Well



Iġnik Sikumi #1

Prudhoe Bay Unit L-pad



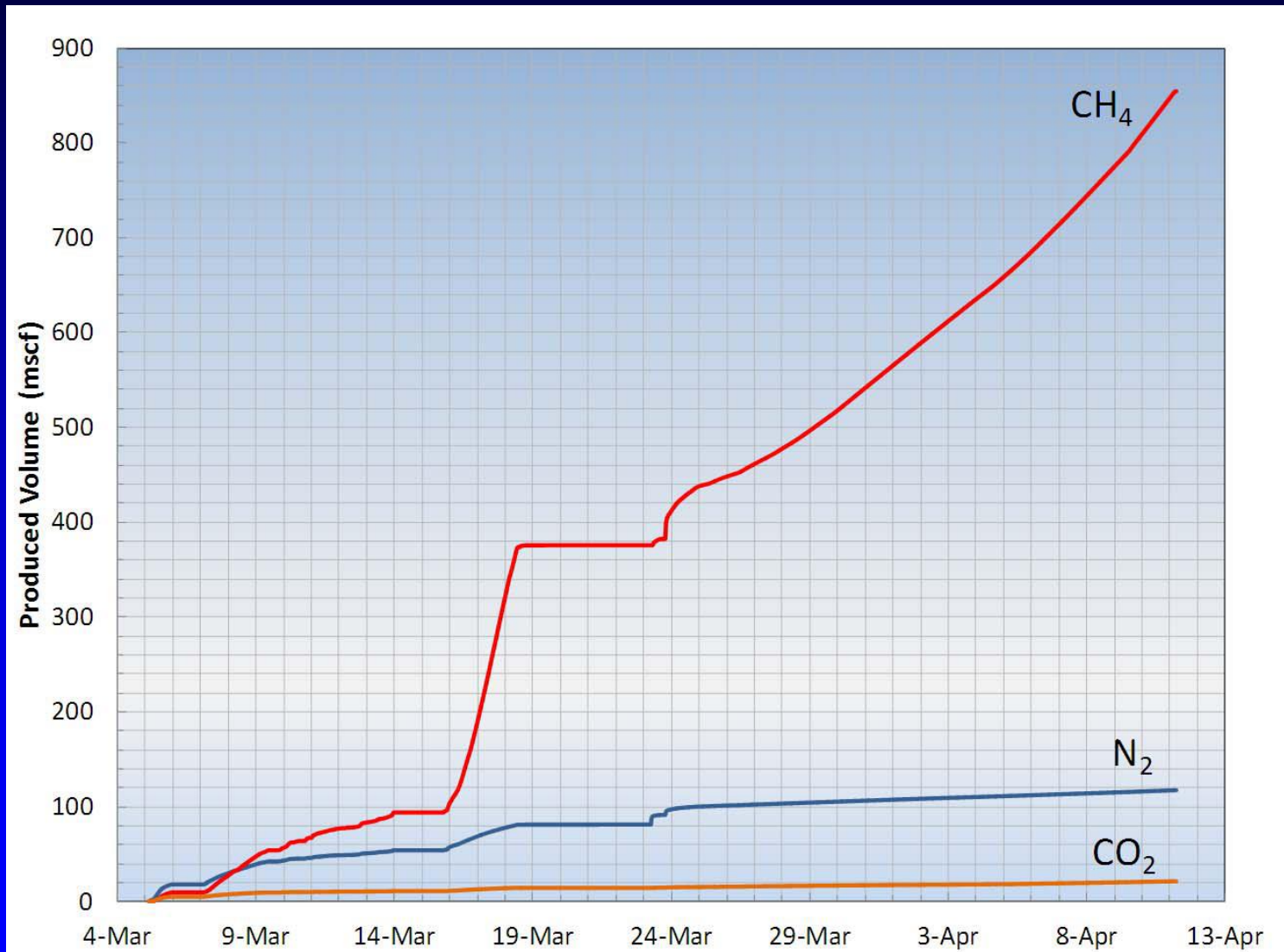


Iḡnik Sikumi #1





Gas Production from the Field Test



Ignik Sikumi #1 Flowback/Drawdown: Gas composition

STATUS

Alaska Field Injection Test 2011-2012

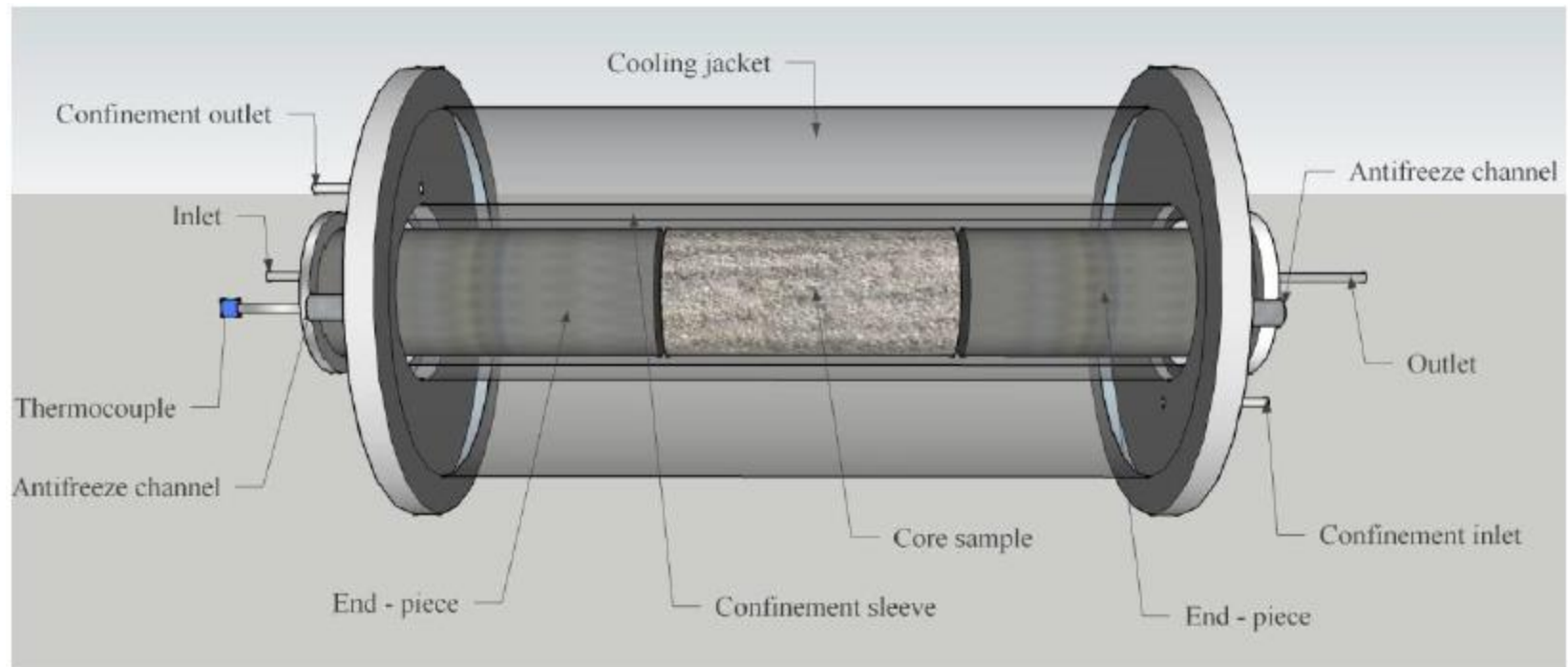
- **ConocoPhillips and JOGMEC**
- **US\$ 11.6 mill funding from US DOE, total cost ca. US\$30mill**
- **CO2 injection**

Core properties

- Bentheim sandstone cores
 - Porosity ~22%
 - Permeability ~1.1 Darcy
 - Grain density ~2.65 g/cm³
 - Mineralogy ~95% quartz



Experimental design



Hossainpour (2013)

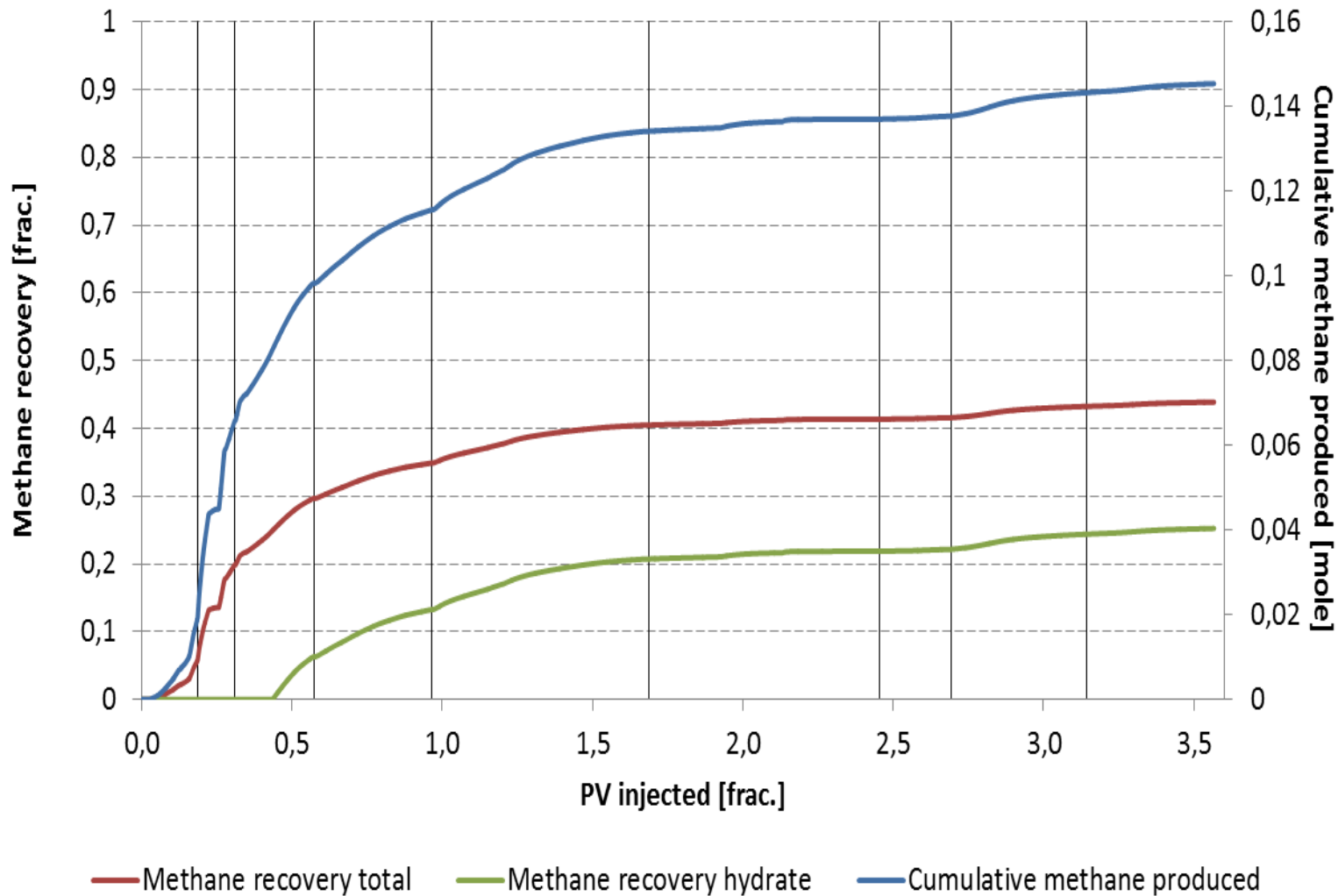
Hydrate formation

- Pressure: 83 bar
- Temperature: 4.0 °C
- Initial brine salinity: 3.5 wt% (NaCl)
- Initial brine saturation: 0.69 [frac.]

- Final brine saturation: 0.31 [frac.]
- Final gas saturation: 0.20 [frac.]
- Final hydrate saturation: 0.49 [frac.]



CH₄-CO₂ exchange



Conclusion

- A binary mixture of 60% N₂ and 40% CO₂ [mole percent] was successfully injected into a hydrate-filled whole core containing excess water. The initial rate of methane recovery from hydrates was high but had a rapid decline.



How will the unconventional gas boom affect prices in other markets?

Average natural gas prices by region, May 2012



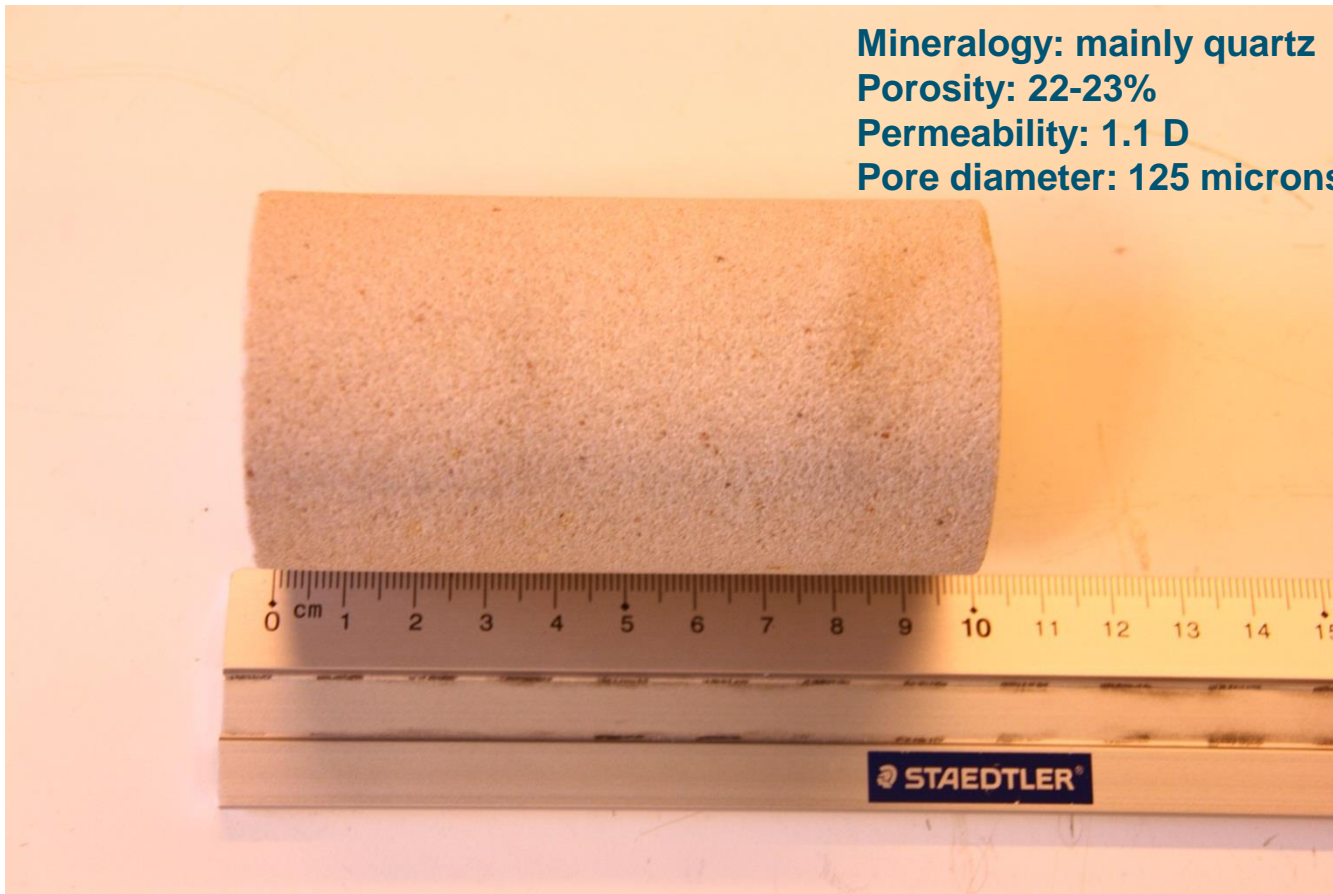
Unconventional gas boom will spur a degree of convergence in global prices by putting pressure on oil-price indexation of gas contracts in Europe & Asia

Thank you!

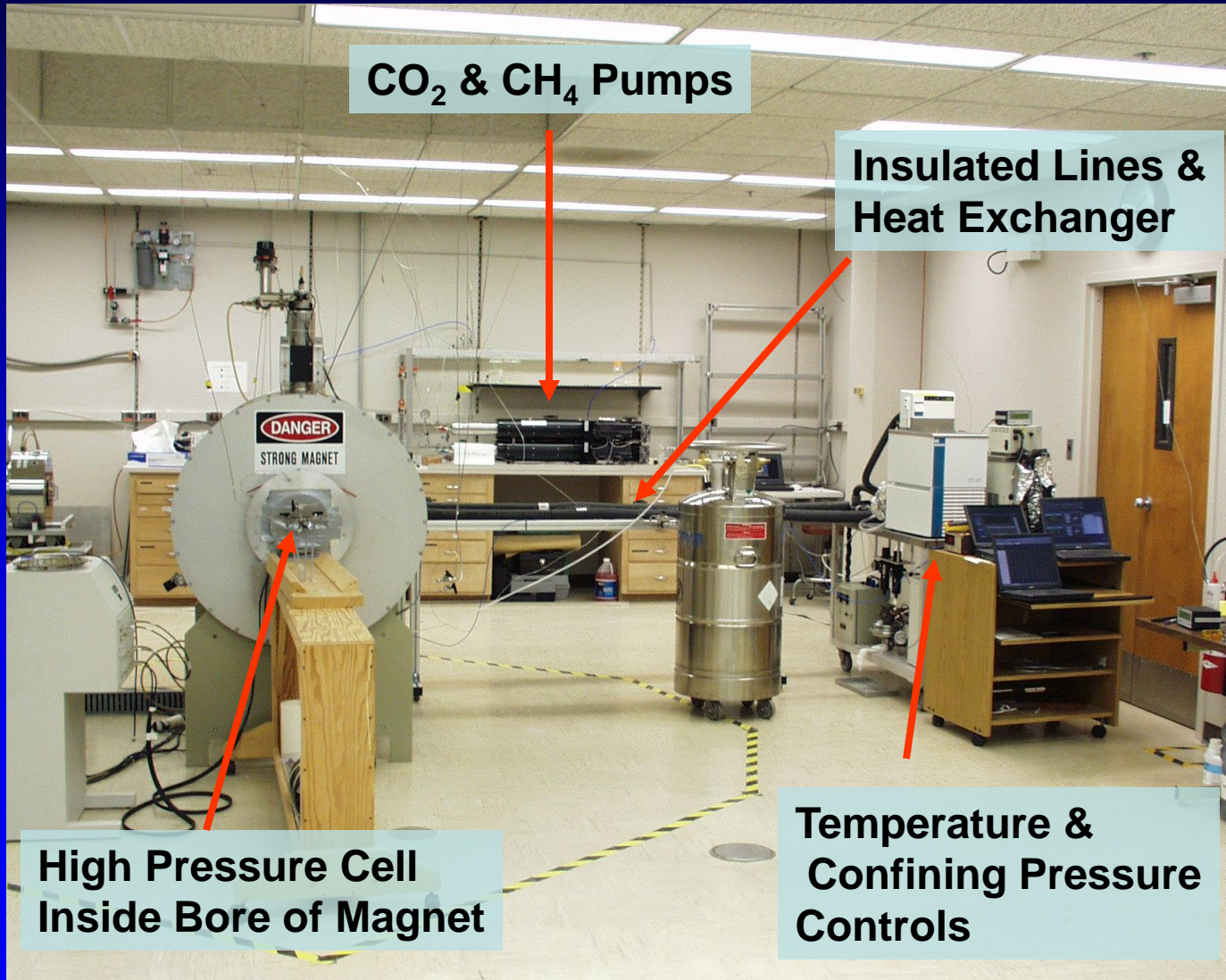
CONDITIONS OF A HYDRATE RESERVOIR

- Hydrate reservoirs are often found in porous media
 - Sedimentary rock

Mineralogy: mainly quartz
Porosity: 22-23%
Permeability: 1.1 D
Pore diameter: 125 microns



Experimental Setup



CO₂ & CH₄ Pumps

Insulated Lines & Heat Exchanger

DANGER
STRONG MAGNET

High Pressure Cell
Inside Bore of Magnet

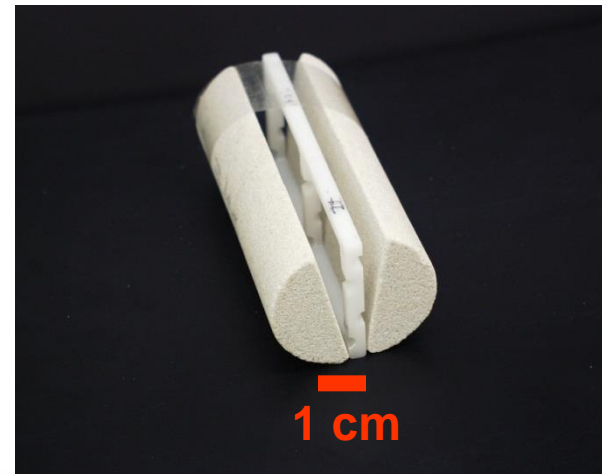
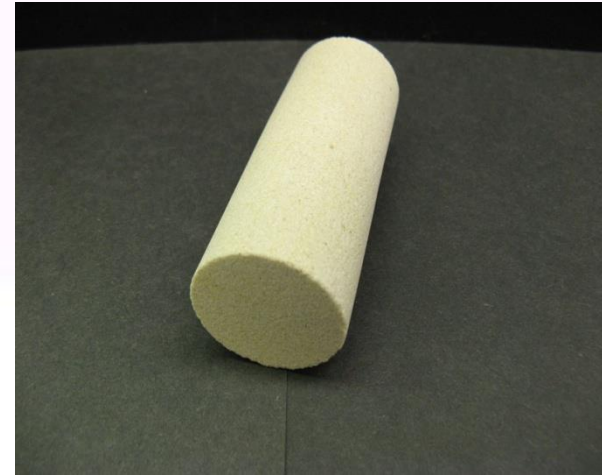
Temperature &
Confining Pressure
Controls

Core Sample Design

Bentheim Sandstone

20-25% porosity, ~ 1.1 D Perm

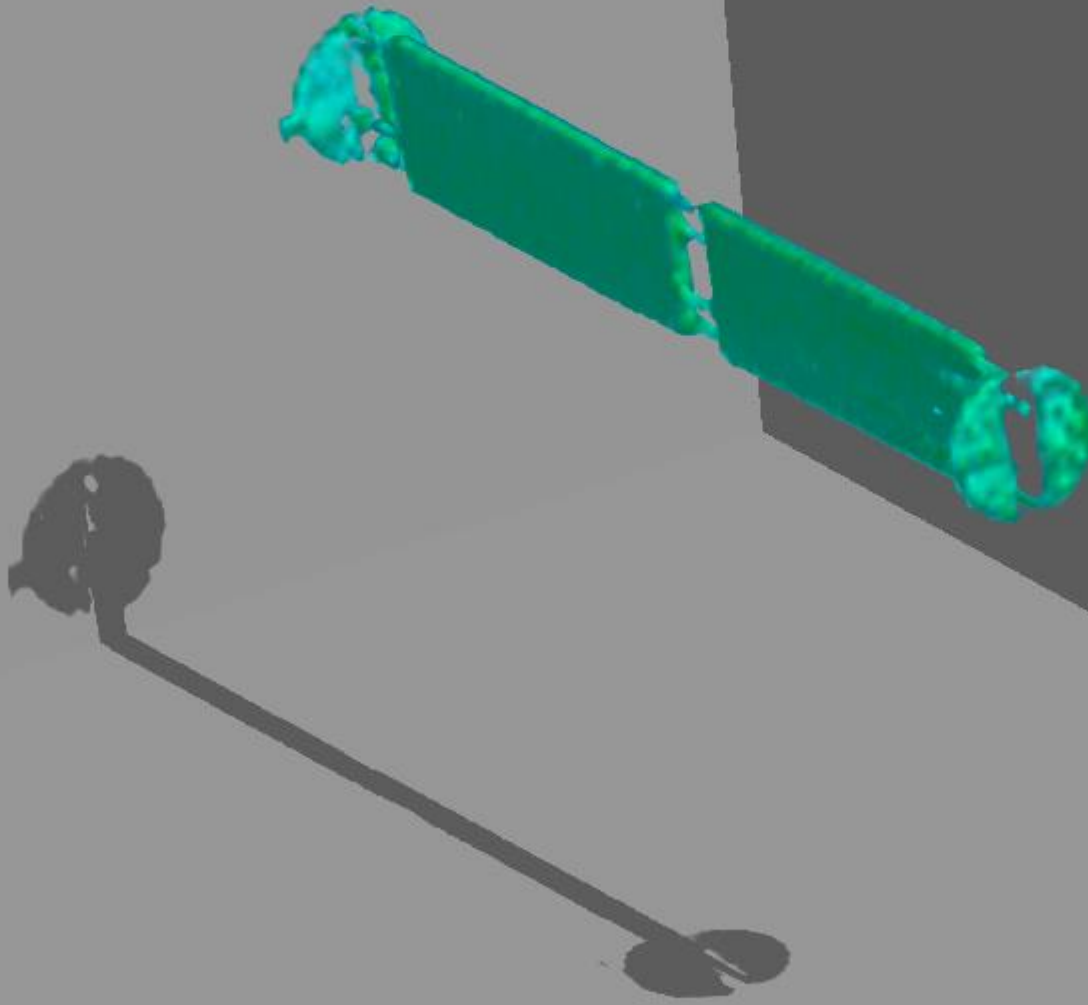
- Whole Core
- Longitudinal Cut With Machined Spacer to Simulate Open Fracture.



33-03

0.0 hrs

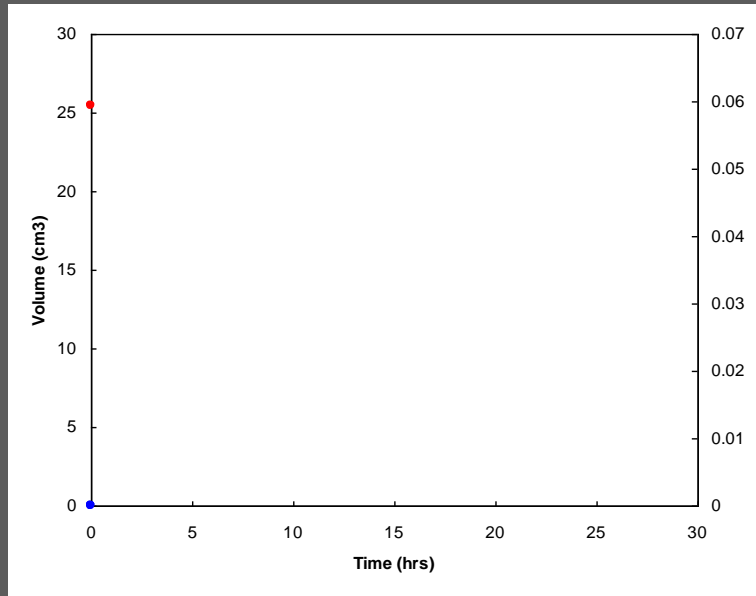
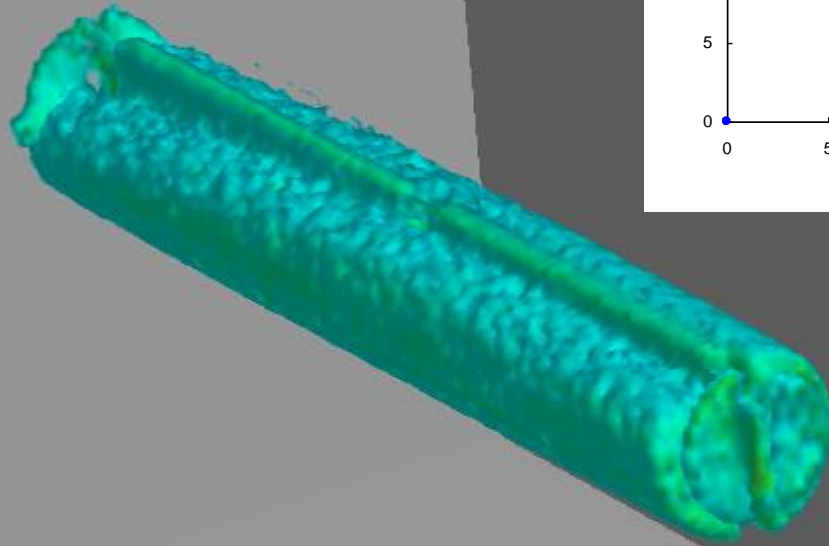
Methane in Spacer



33-07

0.0 hrs

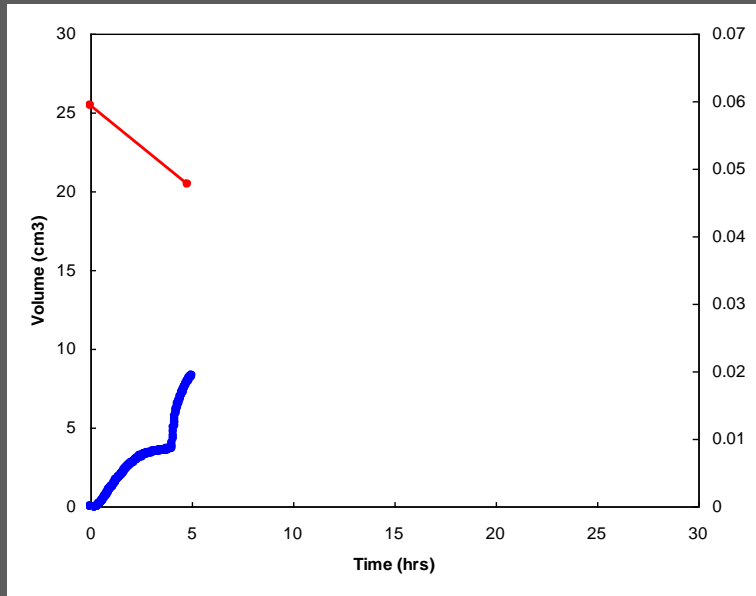
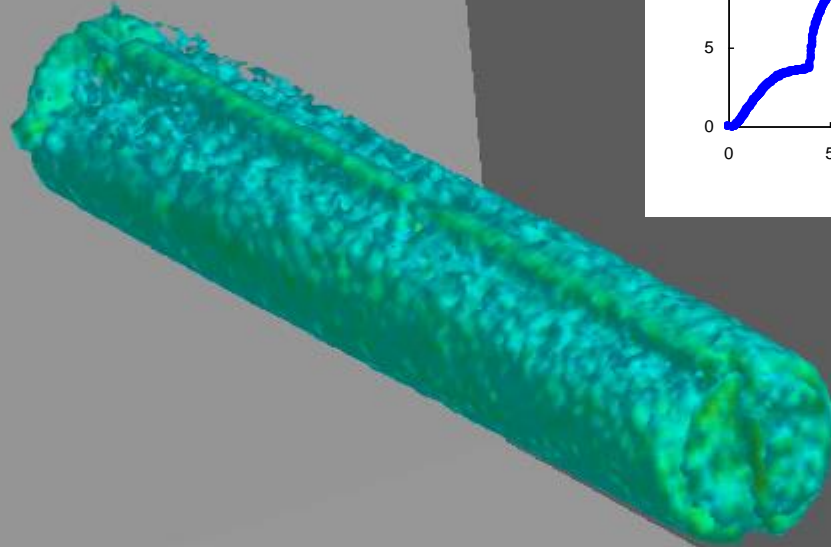
Sw=0.5 + Methane



33a-01

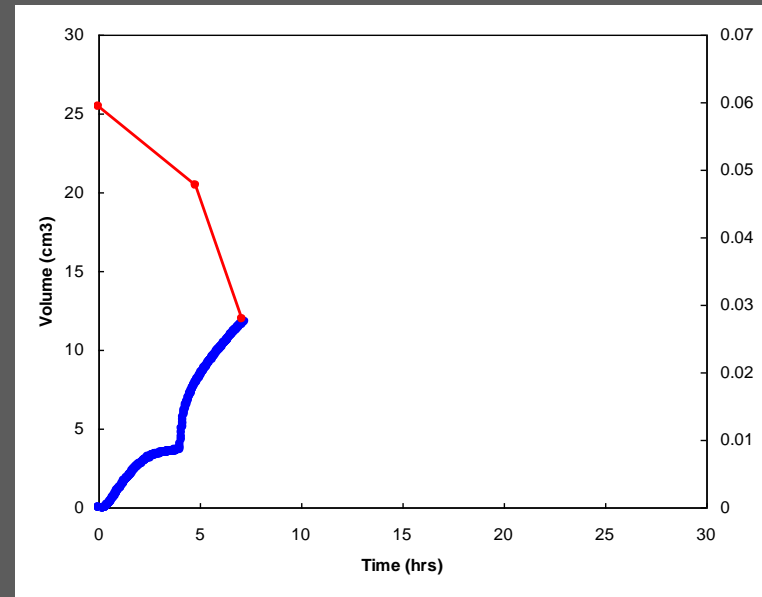
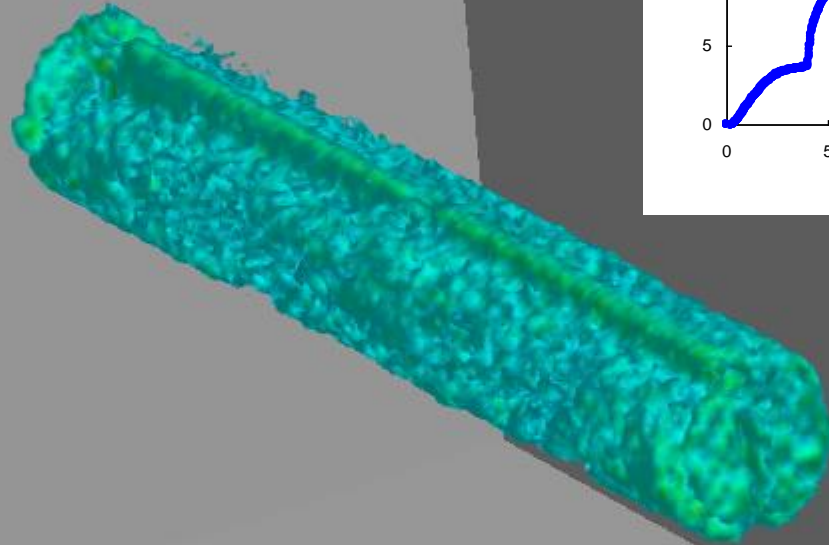
5.0 hrs

Cooling Starts



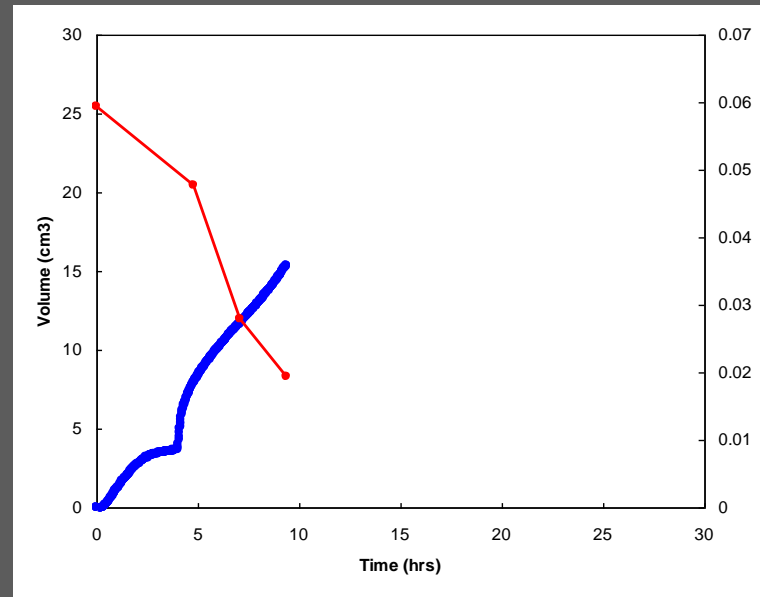
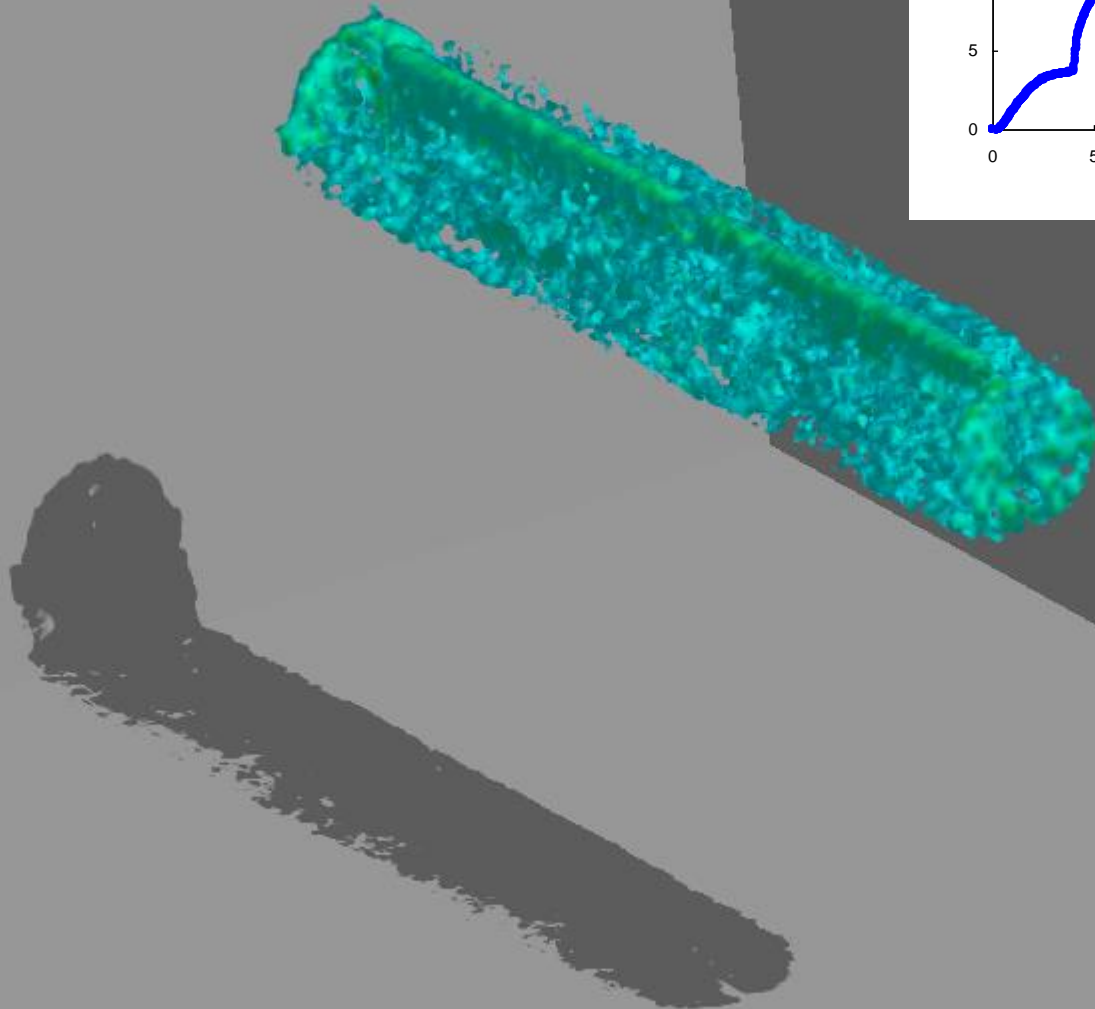
33c-01

7.2 hrs



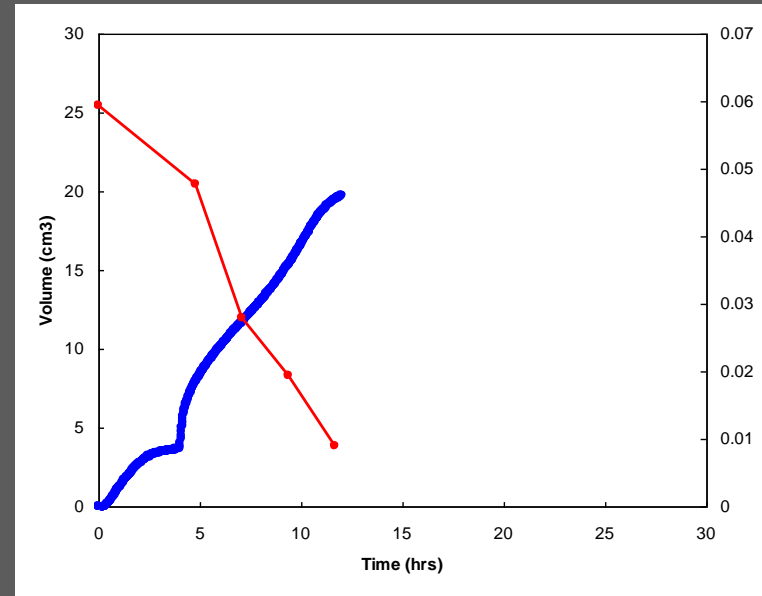
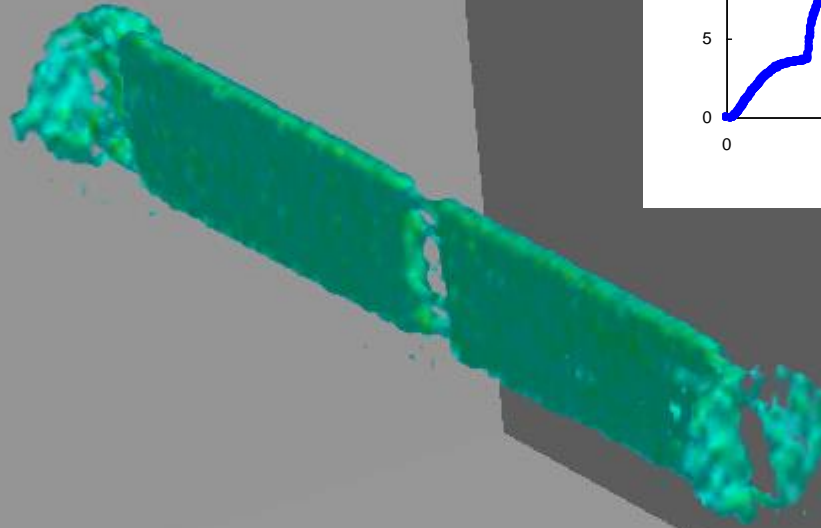
33c-02

9.4 hrs



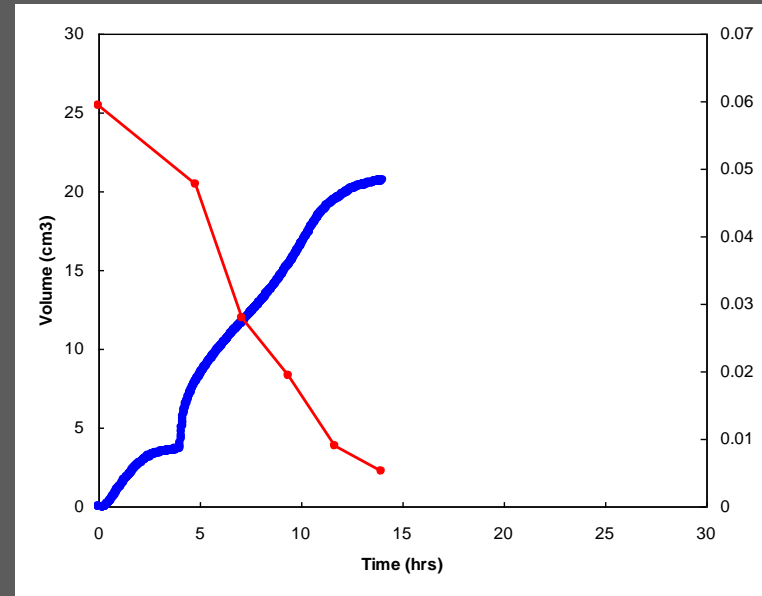
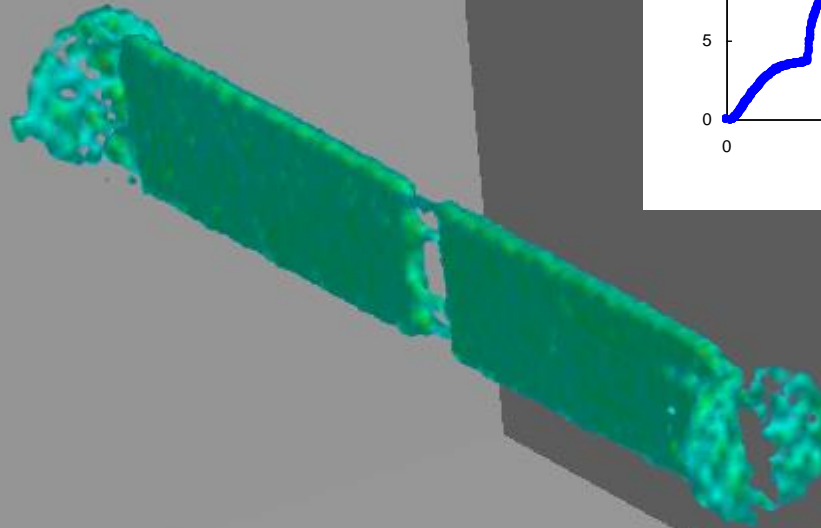
33c-03

12.0 hrs



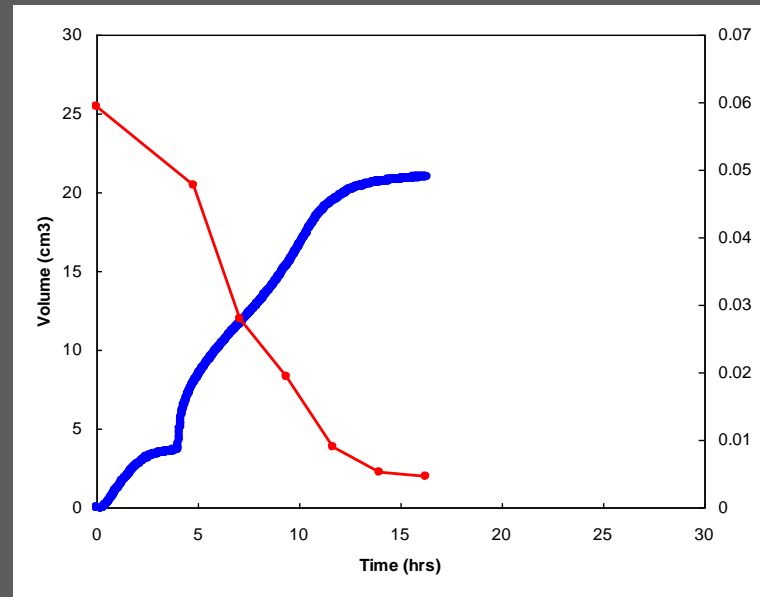
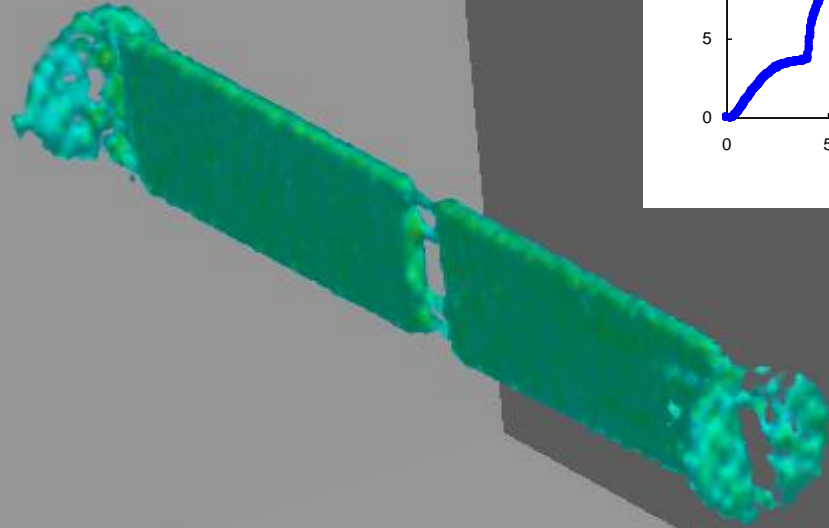
33c-04

14.0 hrs



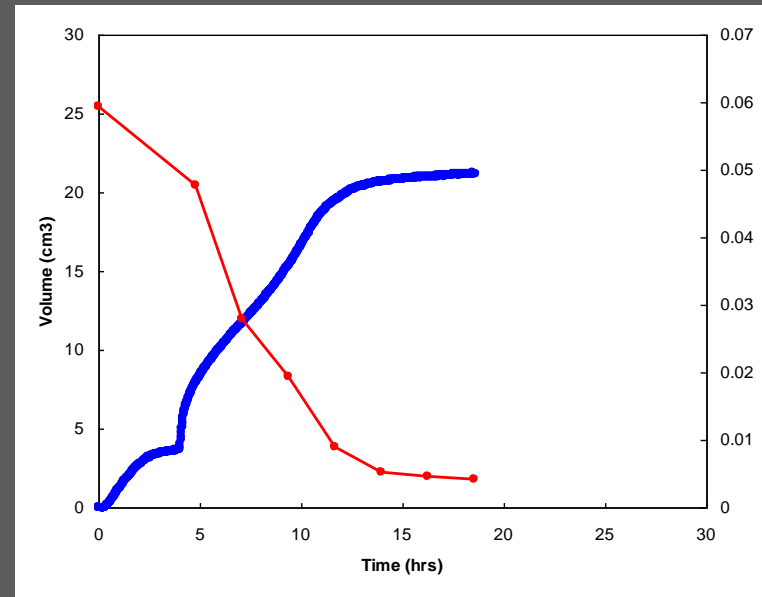
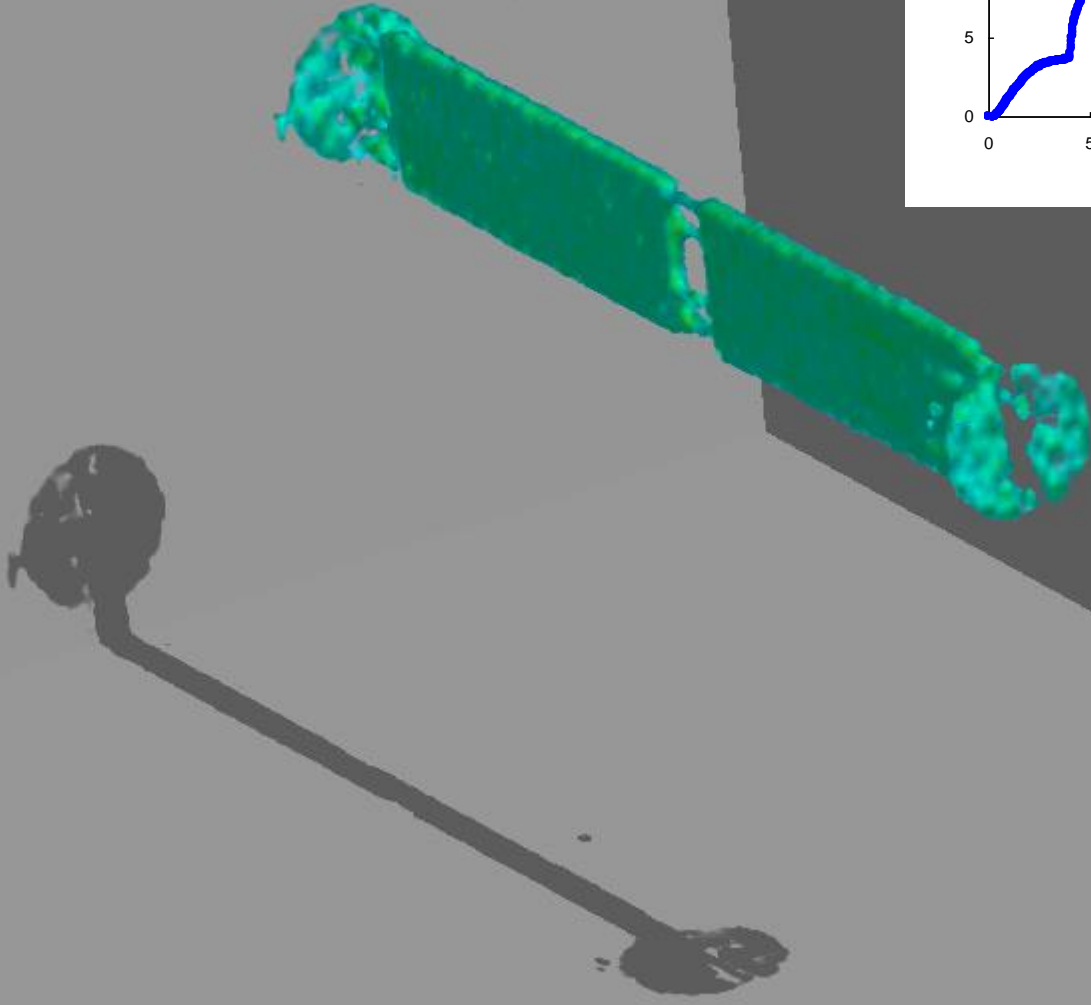
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16.3 hrs



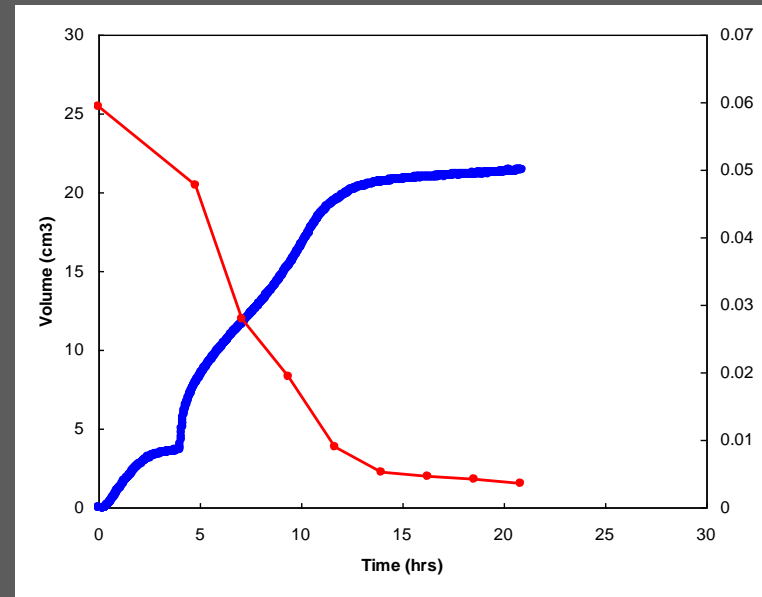
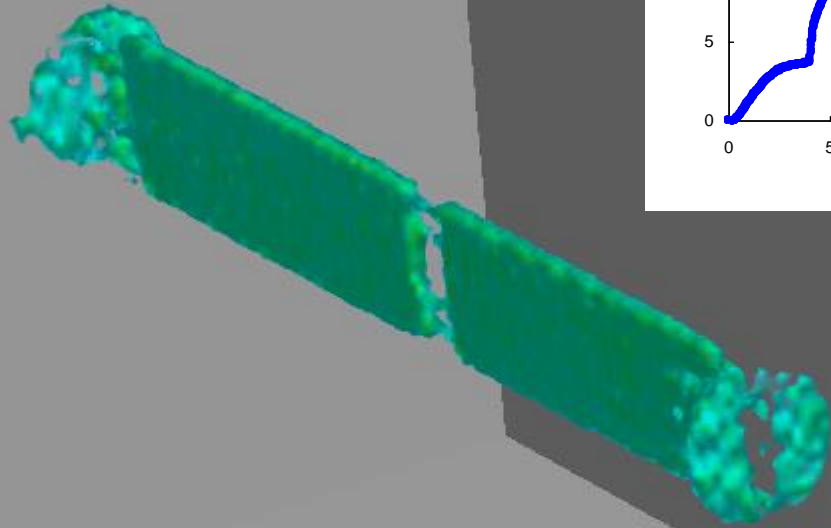
33c-06

18.6 hrs



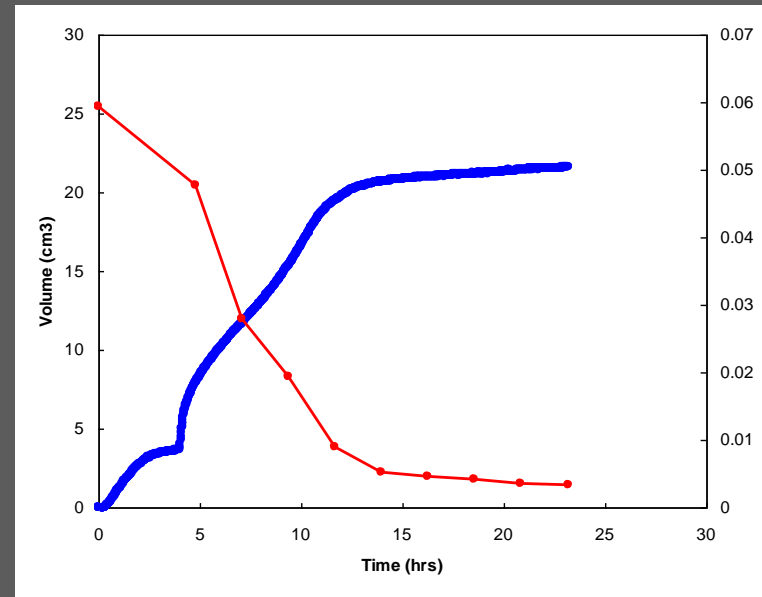
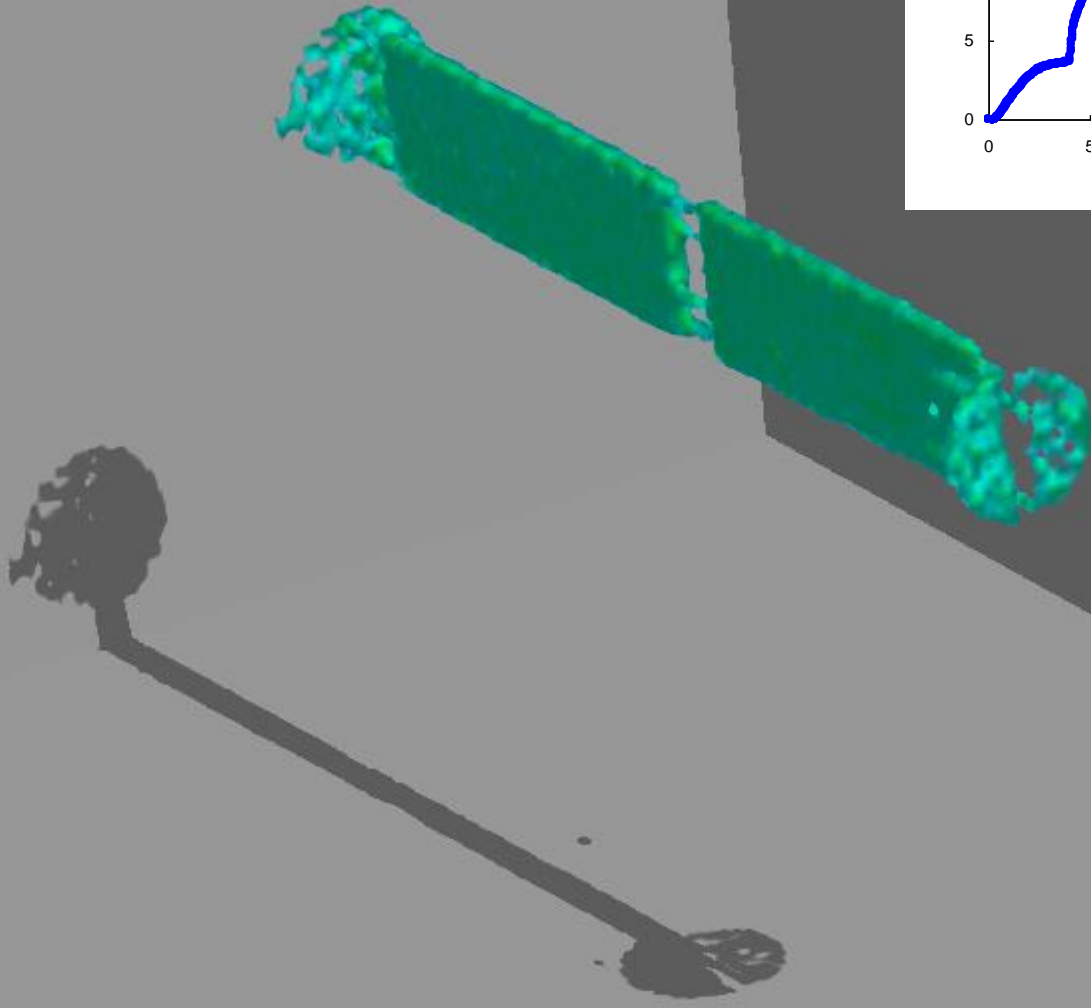
33c-07

20.9 hrs



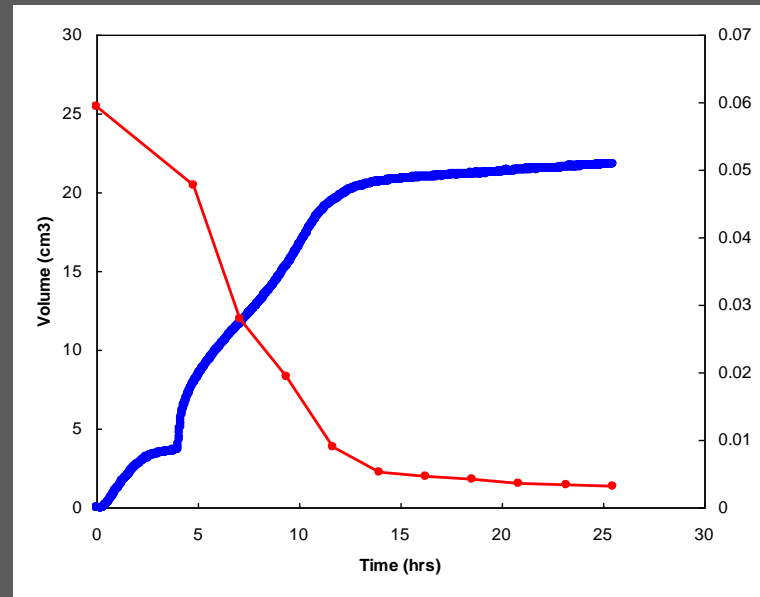
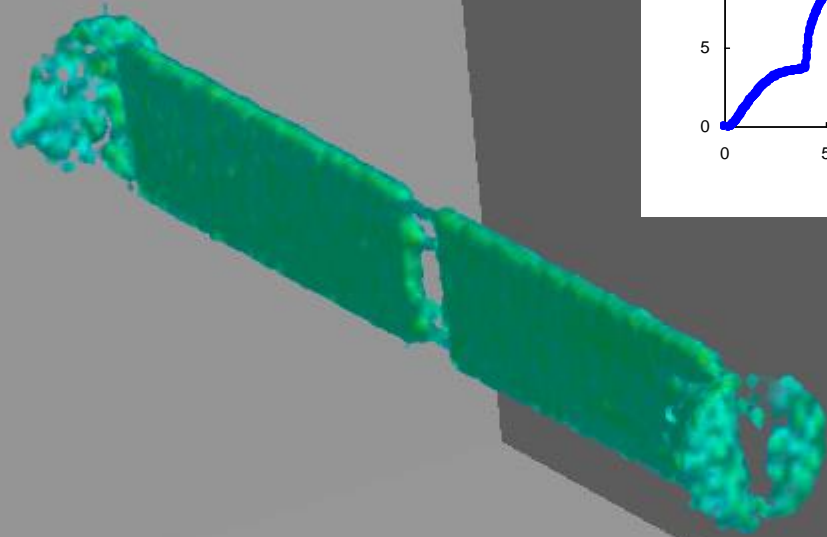
33c-08

23.2 hrs



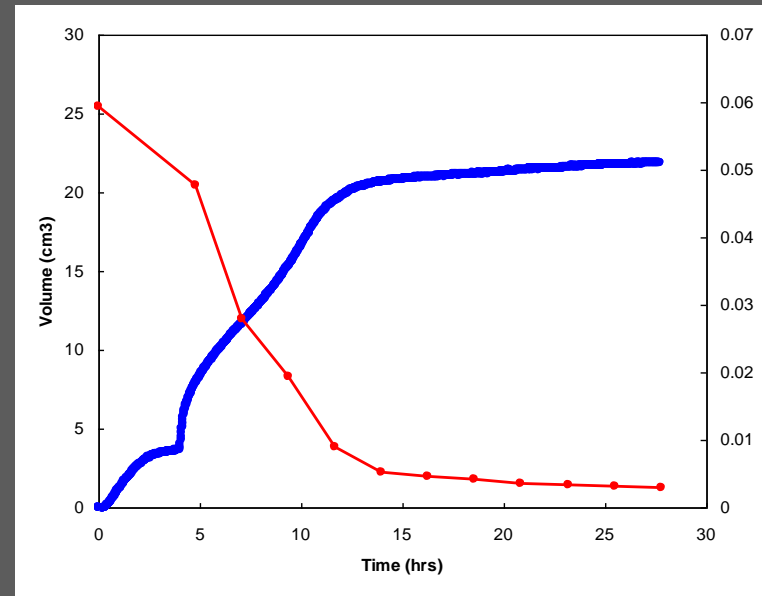
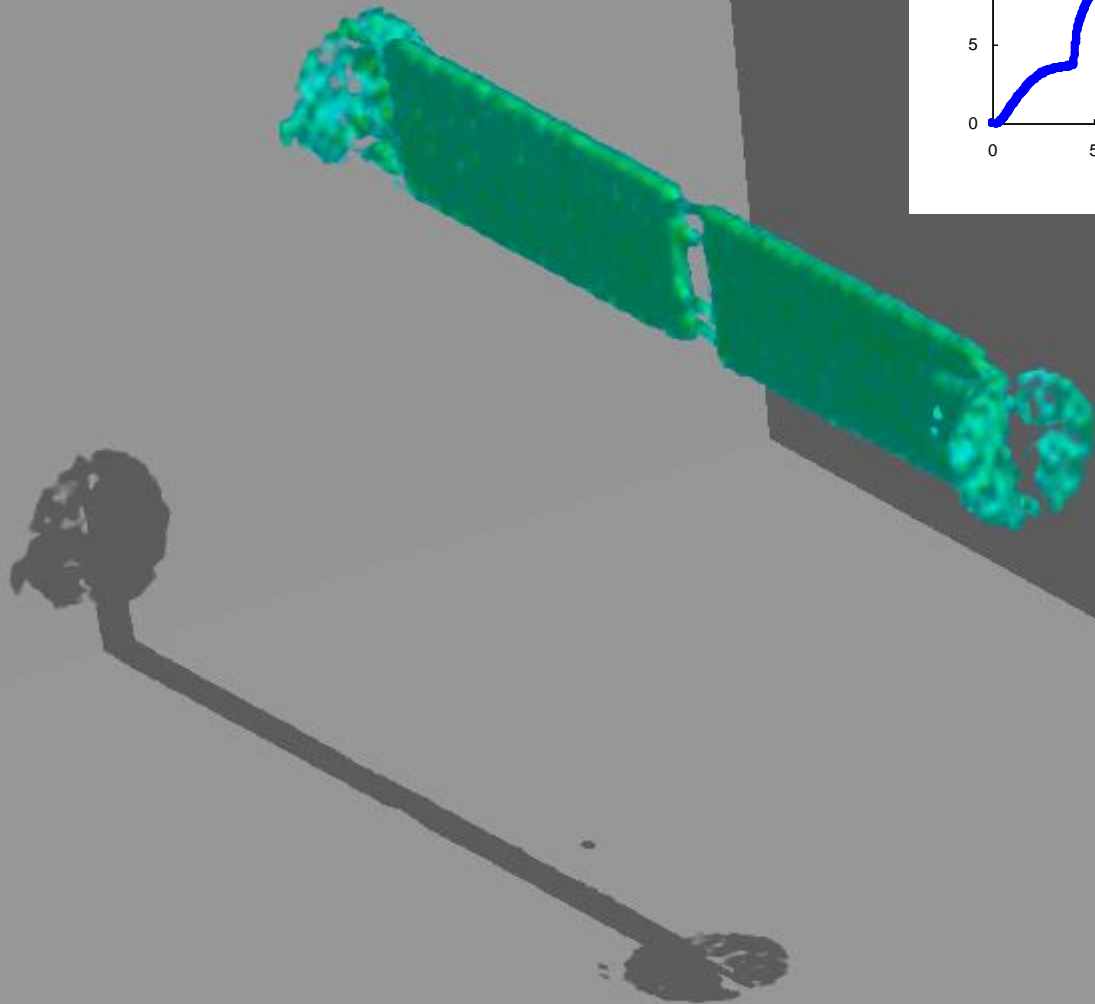
33c-09

25.5 hrs



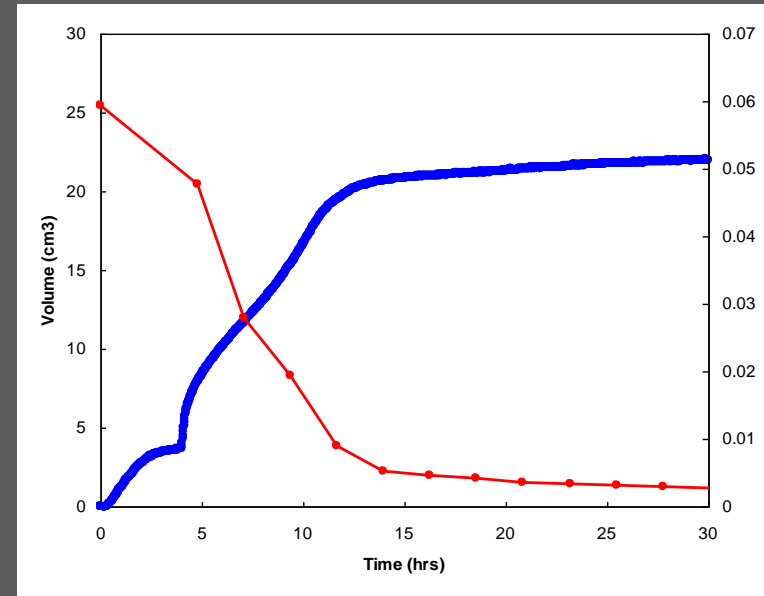
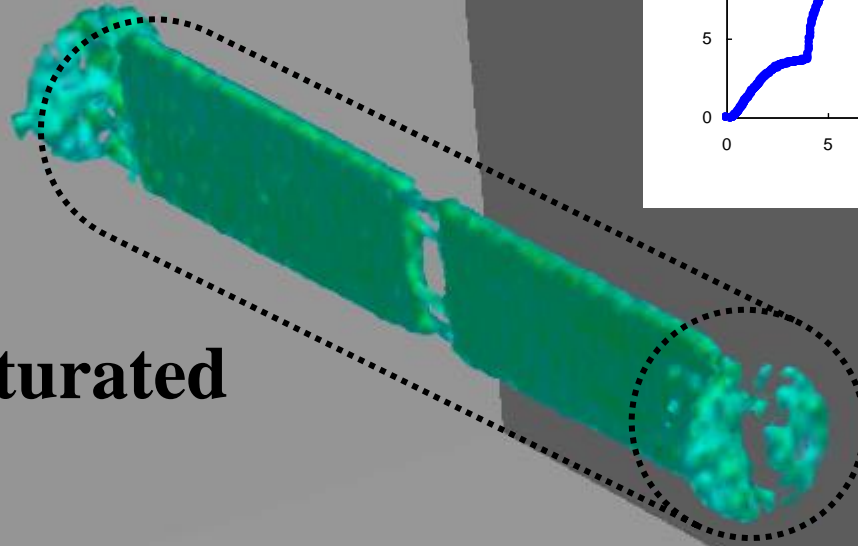
33c-10

27.7 hrs



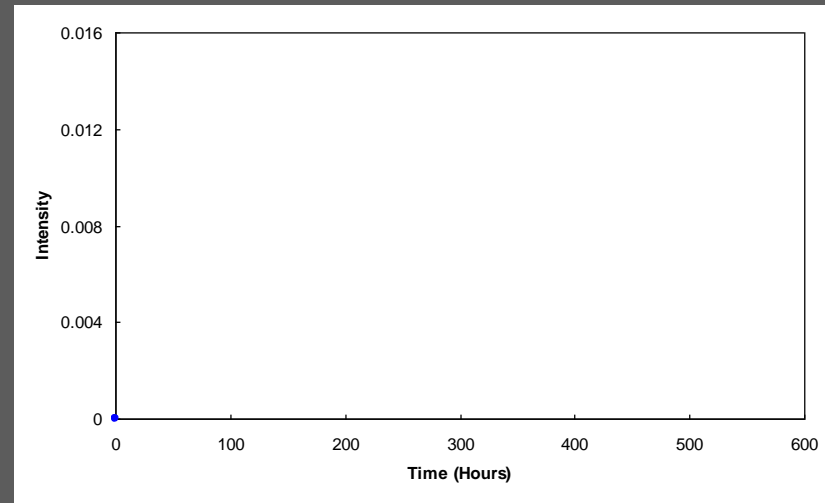
33c-11

30.0 hrs



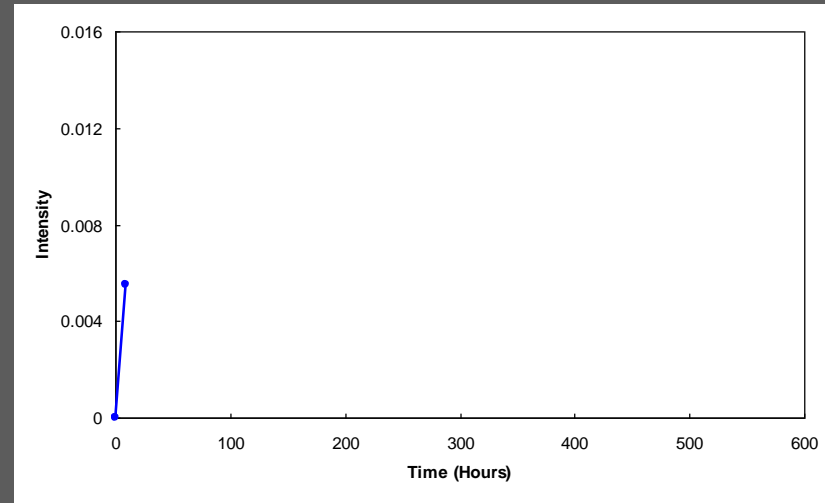
**Core Halves Saturated
with hydrate**

0.0 hrs



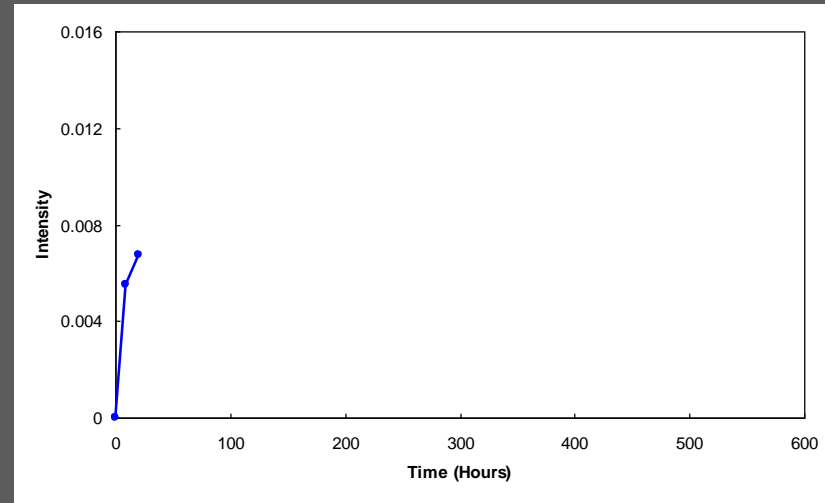
34a-01

9.1 hrs



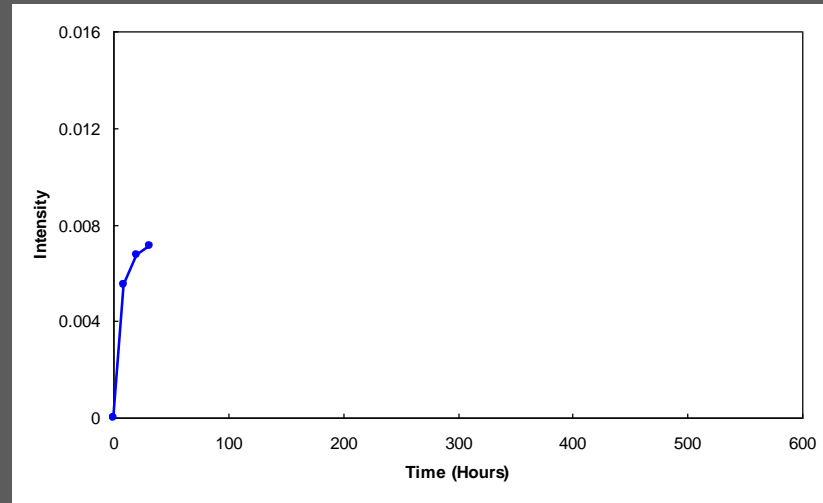
34b-01

20.6 hrs



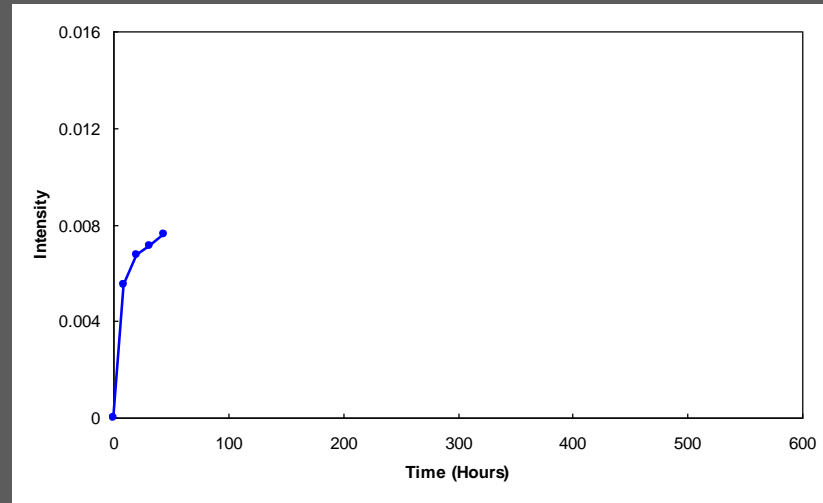
34b-02

32.0 hrs



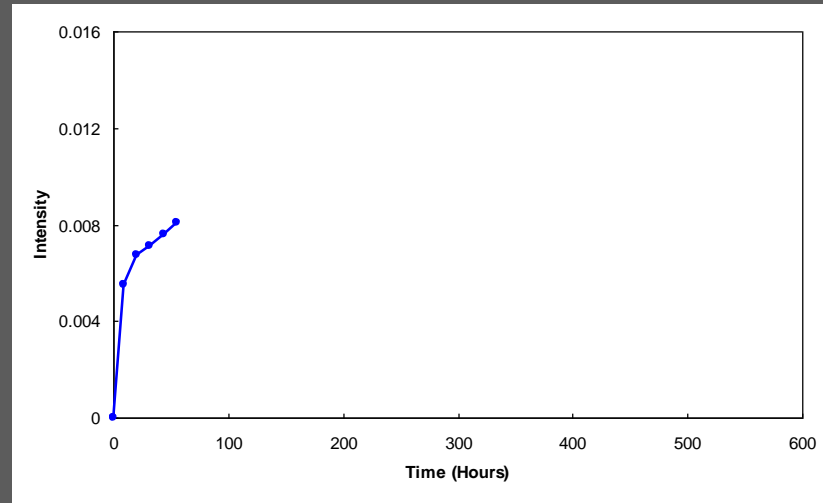
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43.4 hrs



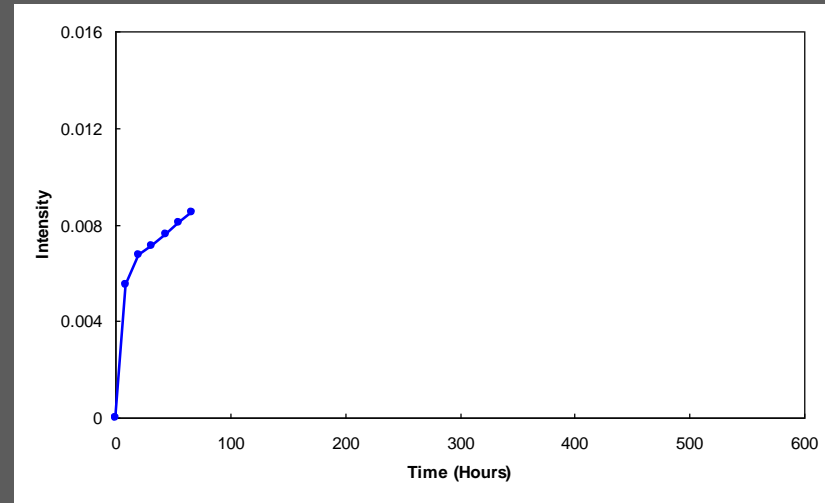
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54.9 hrs



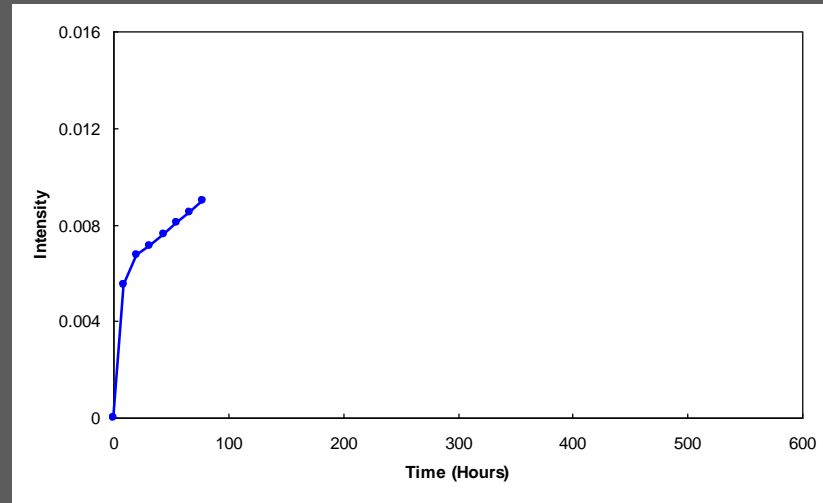
34b-05

66.3 hrs



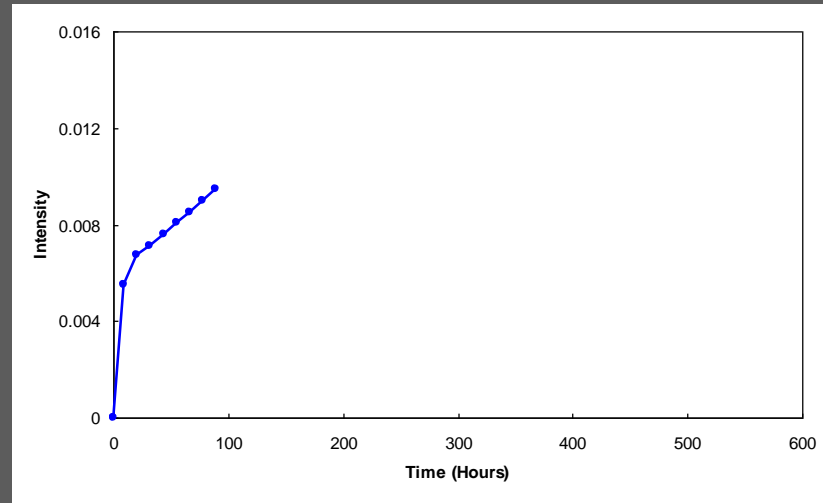
34b-06

77.8 hrs



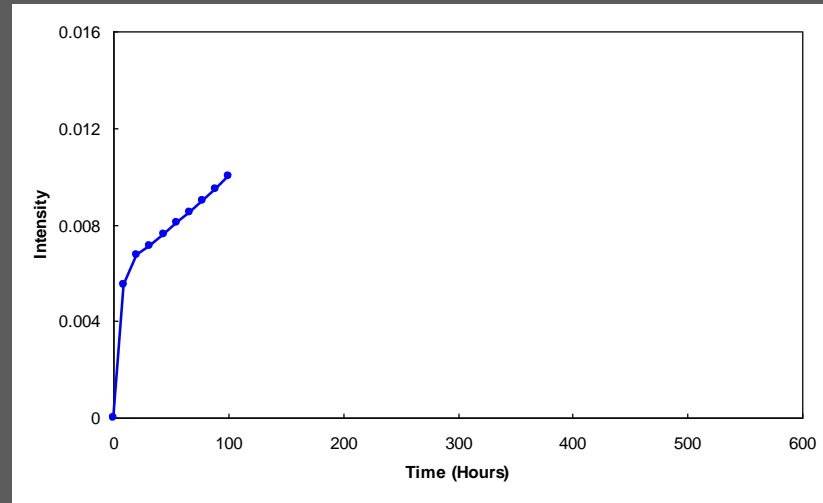
34b-07

89.2 hrs



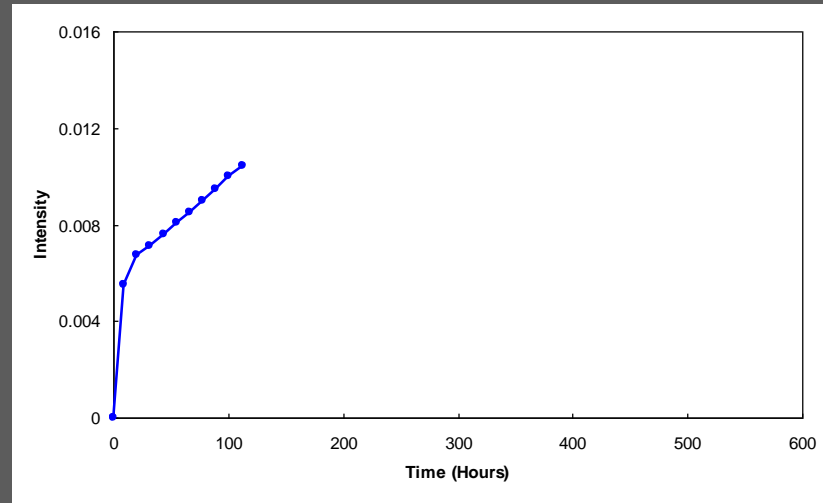
34b-08

100.6 hrs



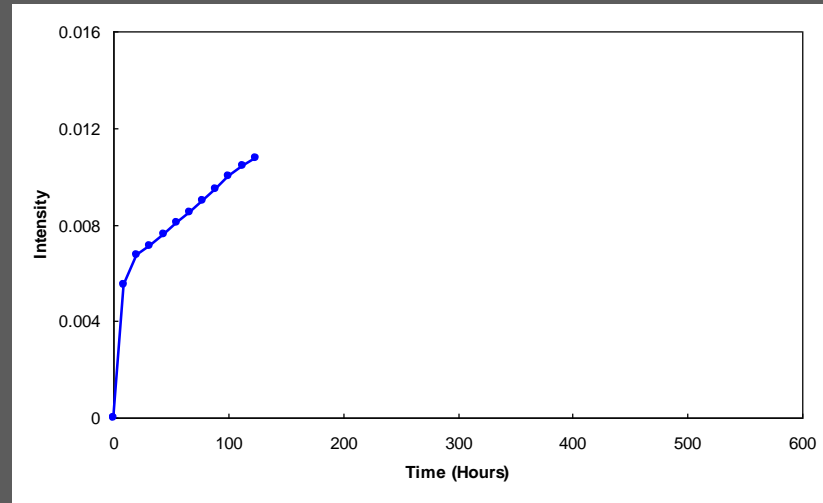
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112.1 hrs



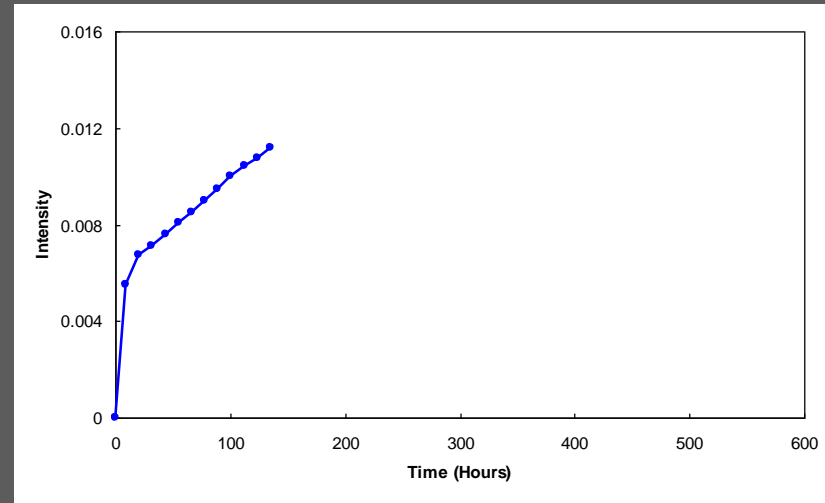
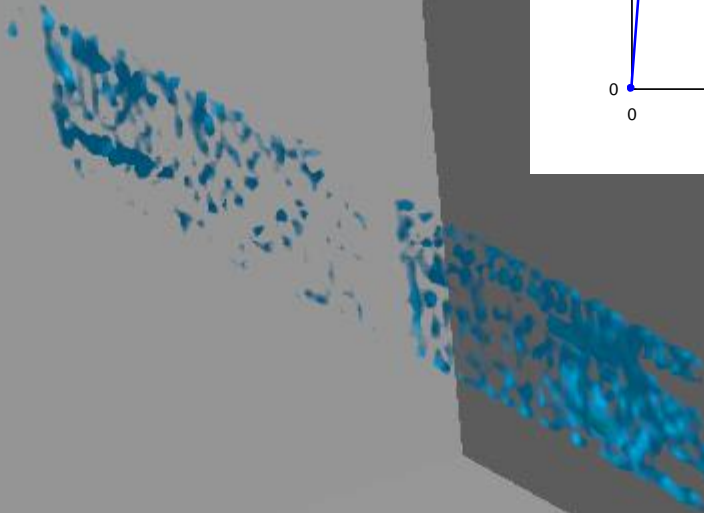
34b-10

123.5 hrs



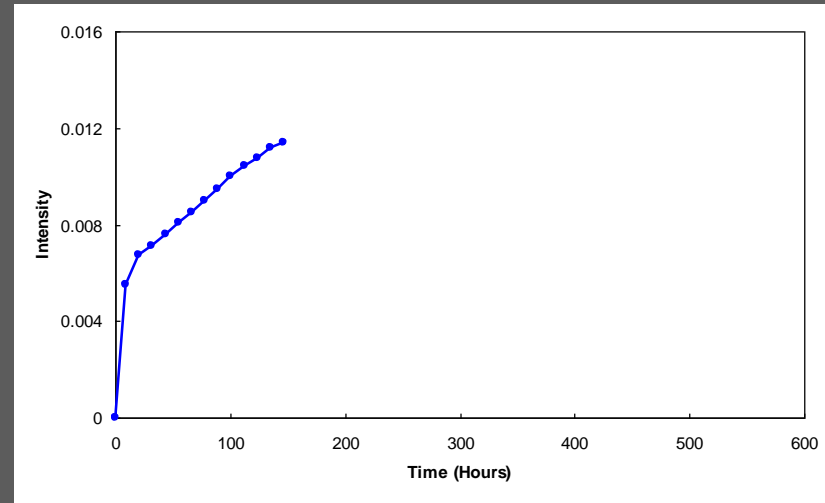
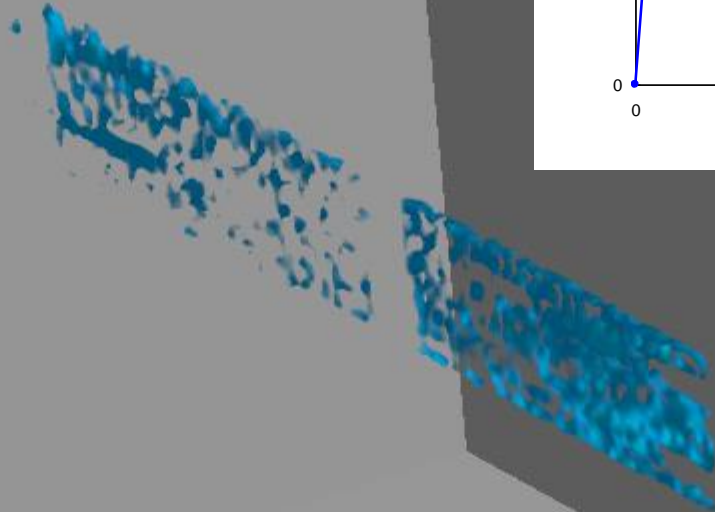
34b-11

135.0 hrs



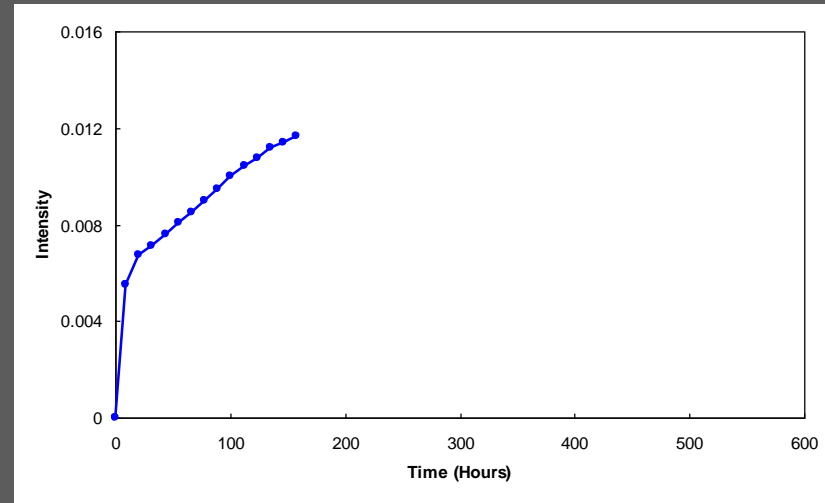
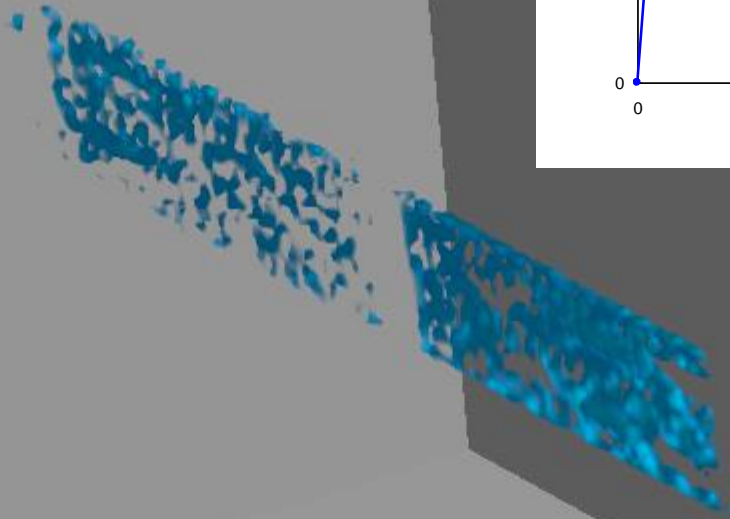
34b-12

146.4 hrs



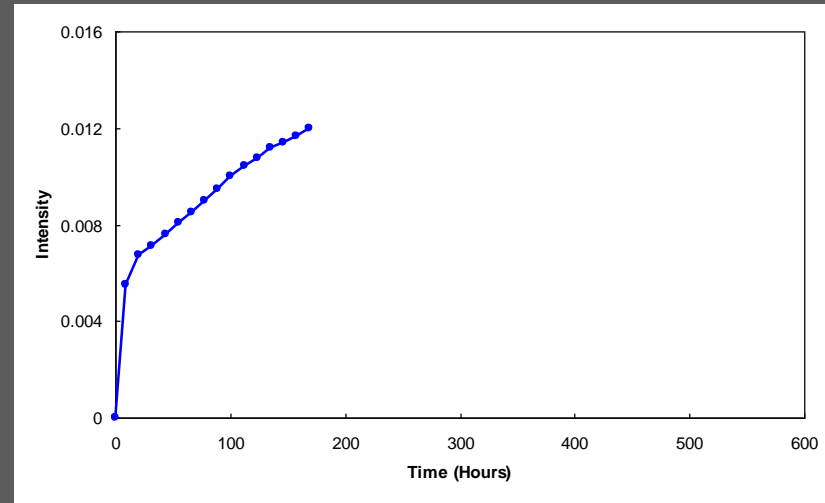
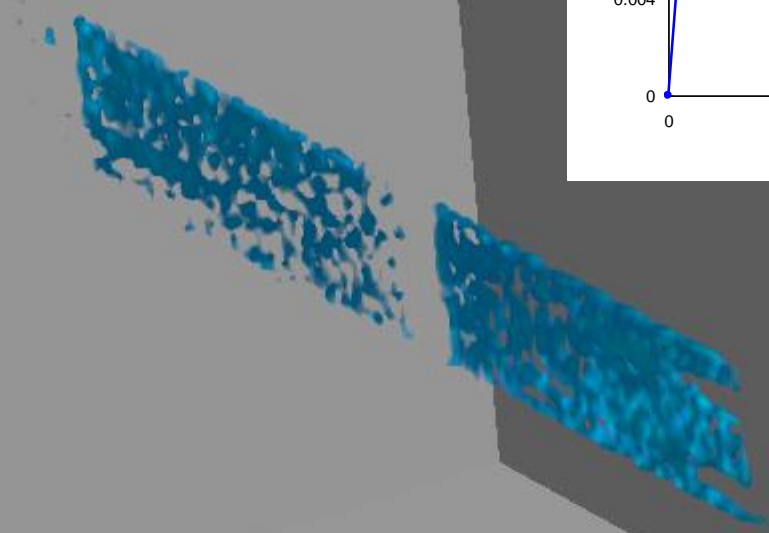
34b-13

157.8 hrs



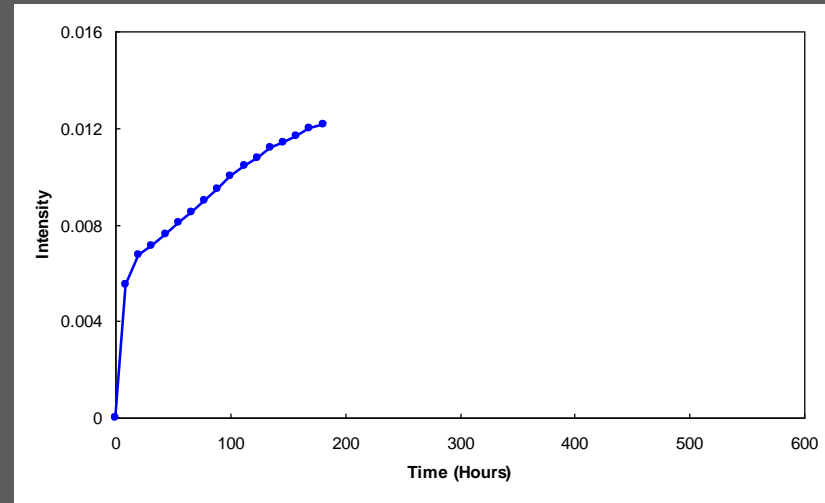
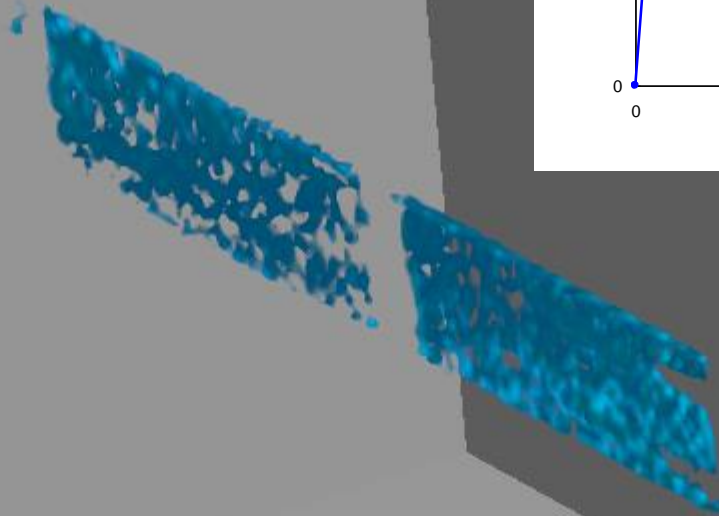
34b-14

169.3 hrs



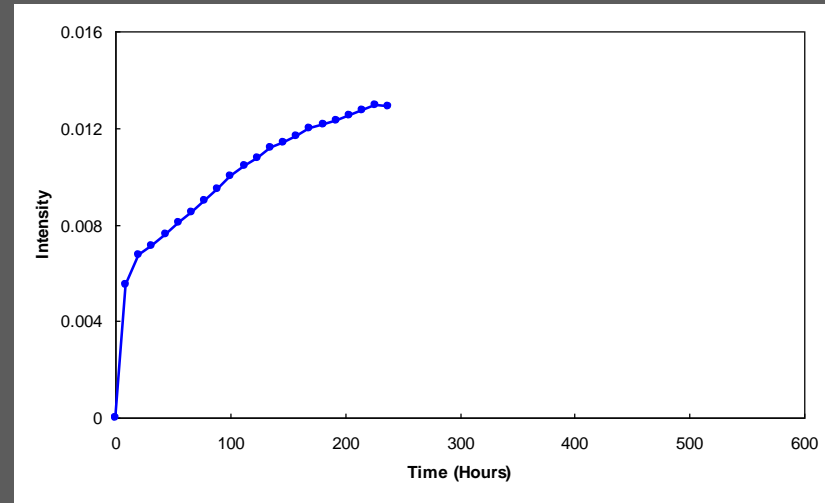
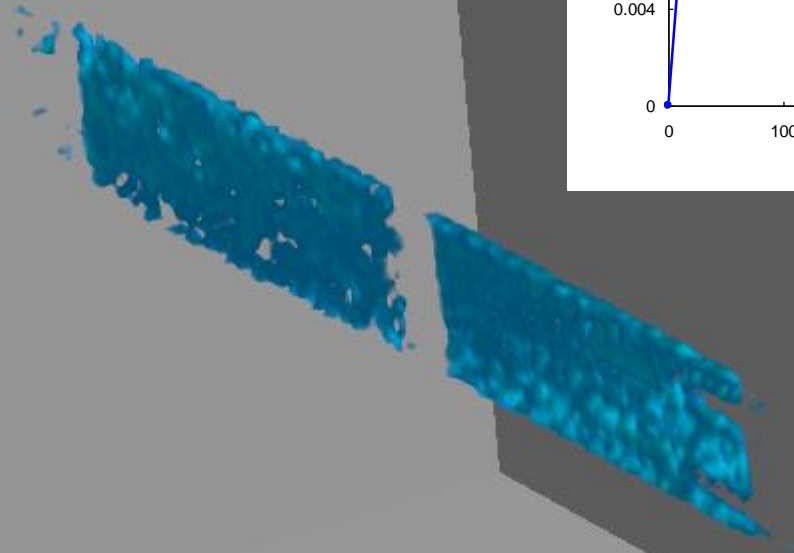
34b-15

180.7 hrs



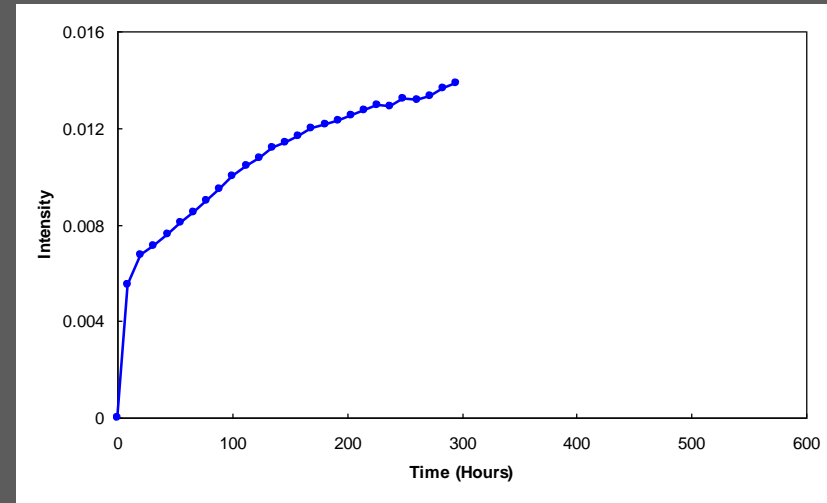
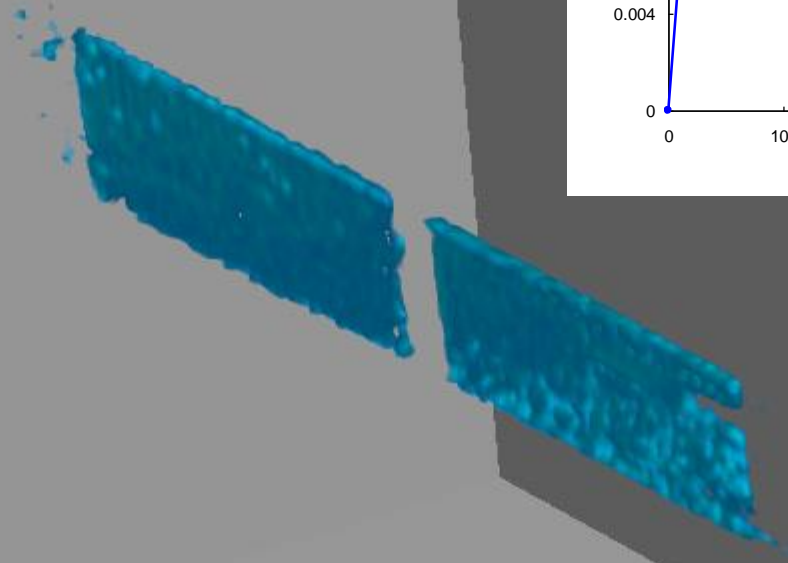
34b-20

237.9 hrs



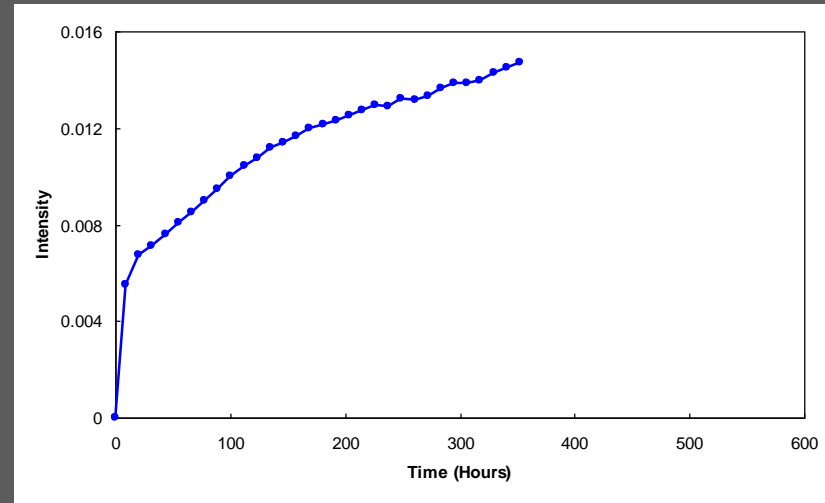
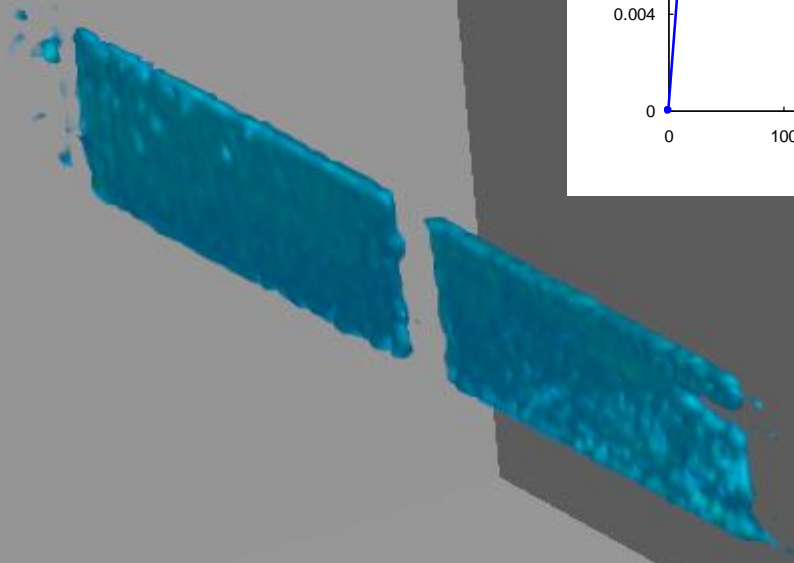
34b-25

295.1 hrs



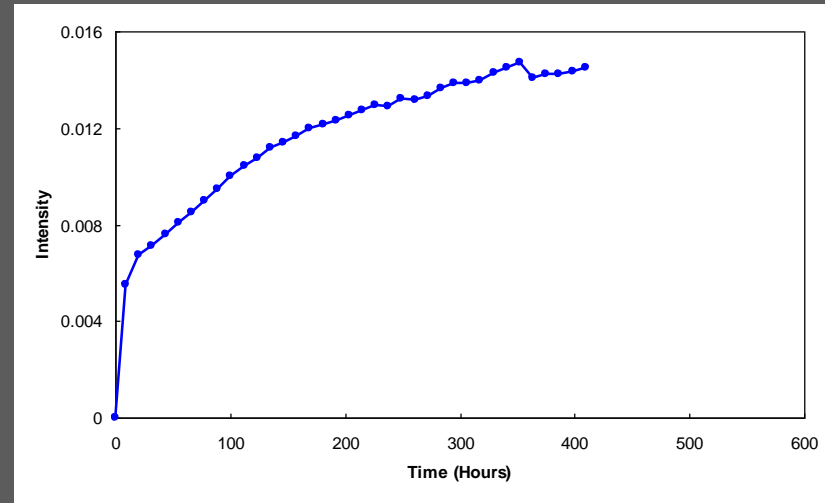
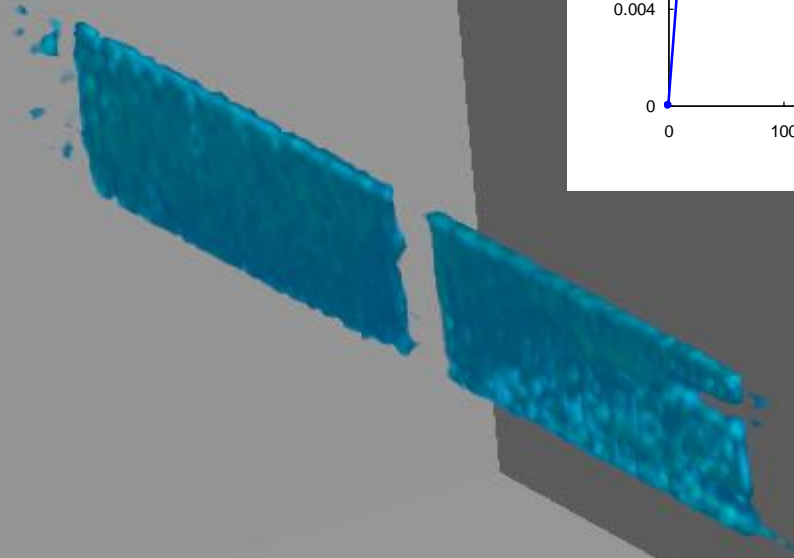
34b-30

352.3 hrs



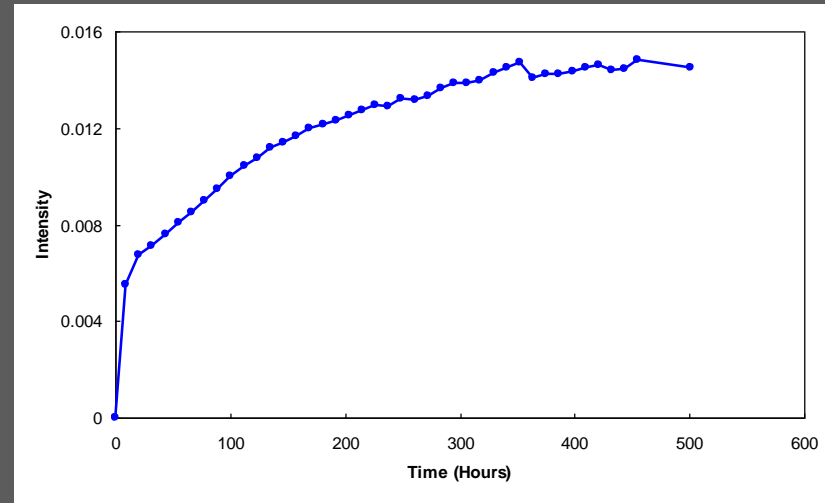
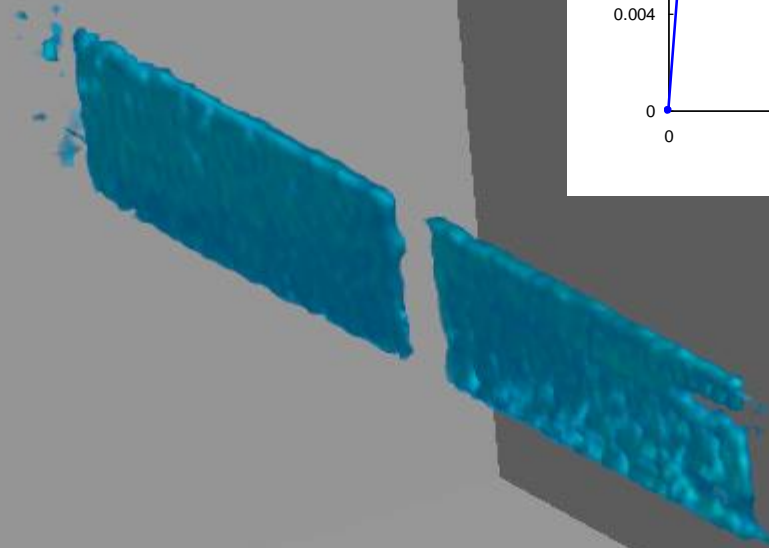
34b-35

409.5 hrs



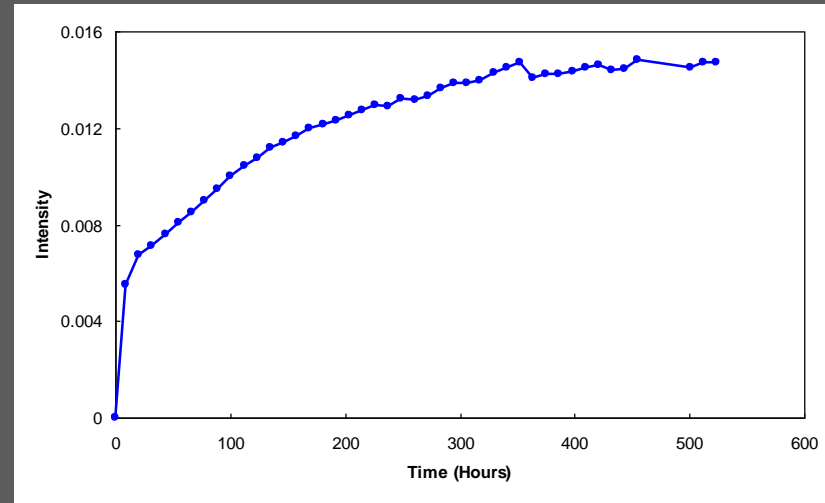
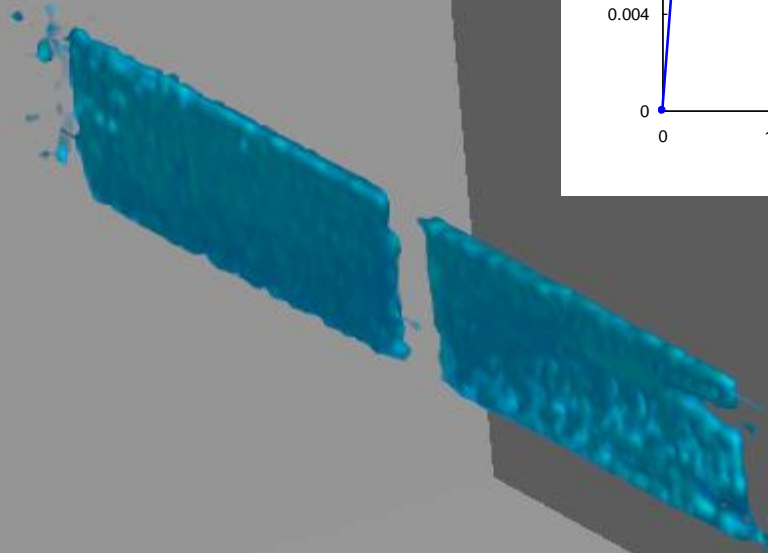
34b-40

501.0 hrs



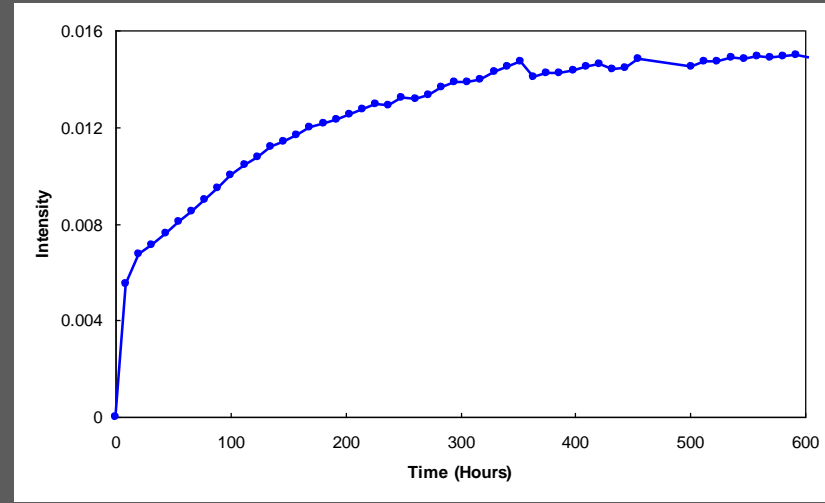
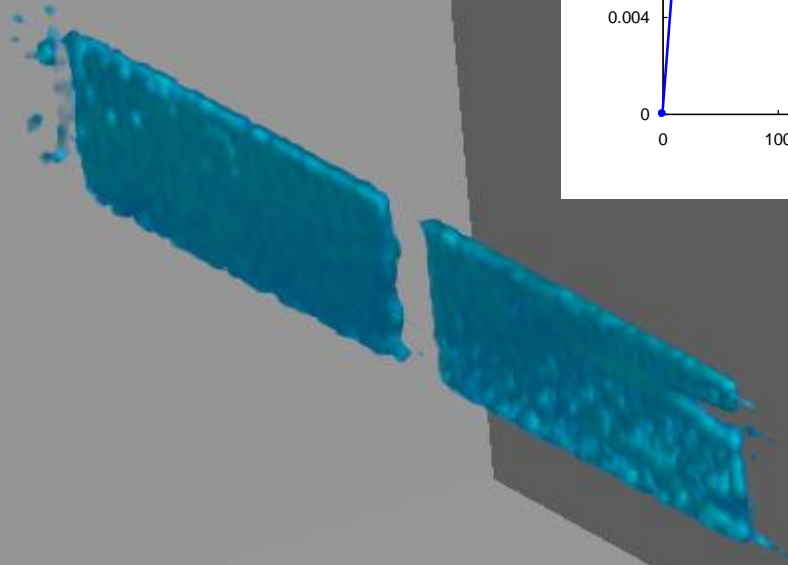
34b-45

523.8 hrs

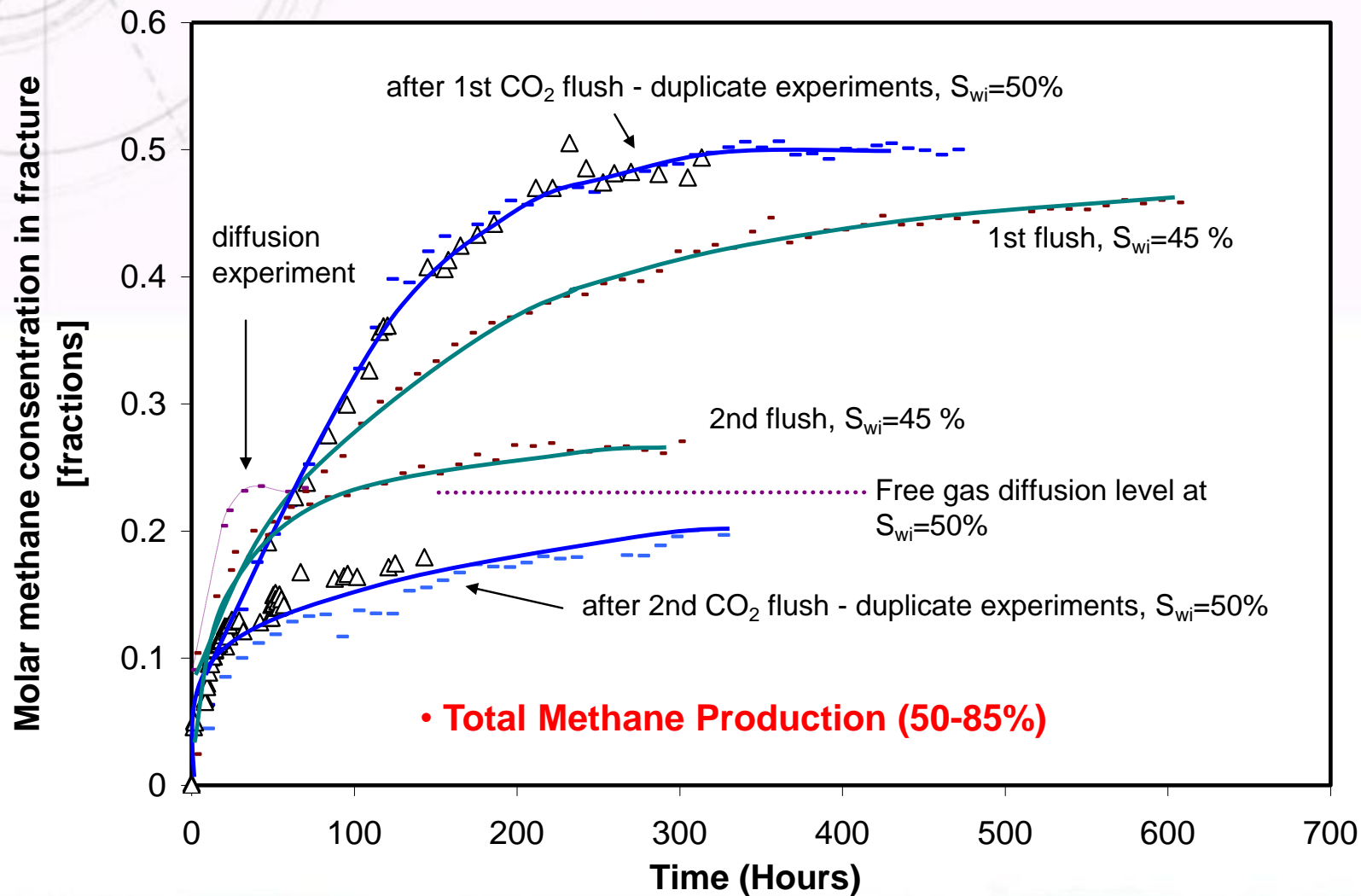


34b-52

603.9 hrs



Methane Production



Thank you!